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Computational Assessment of the Hazardous Release Dispersion from a Diesel Pool Fire in a Complex Building's Area

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Abstract: A hazardous release accident taking place within the complex morphology of an urban setting could cause grave damage both to the population's safety and to the environment. An unpredicted accident constitutes a complicated physical phenomenon with unanticipated outcomes. This is because, in the event of an unforeseen accident, the dispersion of the hazardous materials exhausted in the environment is determined by unstable parameters such as the wind flow and the complex turbulent diffusion around urban blocks of buildings. Our case study focused on a diesel pool fire accident that occurred between an array of nine cubical buildings. The accident was studied with a Large eddy Simulation model based on the Fire Dynamics Simulation method. This model was successfully compared against the nine cubes of the Silsoe experiment. The model's results were used for the determination of the immediately dangerous to life or health smoke zones of the accident. It was found that the urban geometry defined the hazardous gasses dispersion, thus increasing the toxic mass concentration around the buildings.

Keywords: pool fire; urban accident; LES method; FDS model

1. Introduction

An urban environment is an assembly of buildings, parks, commercial and industrial areas, public buildings, and infrastructure such as roads, railways, and airports. The human activity inside the city could cause serious accidents with hazardous release incidents. The air flow distribution and the turbulent diffusion phenomena at the complex environment of a city could result in an unpredictable evolution of an urban accident. This complexity could constitute an impediment to the proper intervention and the accident's management. Therefore, it is important to understand the urban structure and its form, in order to prevent serious toxic release incidences. The main units of an urban environment are the urban building blocks. These define the flow distribution inside the city's environment.

Some field experiments have investigated the pollutant dispersion in a city [1–3]. Yet, field experiments for pollutant dispersion in an urban environment are very difficult and costly. This is the main reason why Computational Fluid Dynamics (CFD) could be a simpler approach for these kinds of studies. Different CFD techniques could be applied to study an urban dispersion problem, such as the Reynolds Average Navier Stokes (RANS) models [4–6], the Large eddy Simulation (LES) models, the Implicit-eddy Large Simulation (ILES) models [7,8] and the Direct Numerical (DNS) models. The air flow within the urban atmospheric boundary layer was also experimentally studied with wind tunnel experiments [9].

In order to define the complex phenomena of an urban geometry, simplified cases for the urban building blocks were studied. The urban building blocks areas can be simplified into arrays with rectangular buildings. Urban building blocks are characterized by buildings' height and the space between them [10,11]. Different studies exist for the study of the flow into elementary urban units such as the street canyons [12–21]; the street intersections [22–24]; the influence of tall buildings in the urban environment [25,26] and in open spaces [27]. Moreover, the flow and pollution dispersion around staggered and aligned groups of cube arrays have been examined [28].

A pool fire accident may occur in a road between urban building blocks. Several studies in an open space pool fire accident exist [29–35], as well as for a pollutant dispersion in a street canyon [17,18,36,37]. However, only a few of them focus on the study of a fire accident inside a street canyon [21,38–42]. The pollutant dispersion into an array of cubes has been studied experimentally and computationally [10,43,44]; however, there is a lack of documentation for a fire incident inside an array of cubes.

The current study presents appropriate computational techniques for the prediction of a toxic release in an urban environment after a fire accident. It also presents a qualitative and quantitative analysis for different urban geometries to predict the immediately dangerous to life or health (IDLH) smoke zones. A Large eddy Simulation technique is applied and defined in Section 2. The simulation's results are discussed in Section 3. Finally, the conclusions are in Section 4.

2. Computational Characteristics

2.1. Flow Field Definition

A simplified urban domain model of nine cubes in different rectangular staggered arrays was studied as is shown in Figure 1. This cube's arrangement is similar to the Silsoe cube arrays research site [45,46]. In Figure 1a, the D2 cube is the Silsoe cubical building. The surface pressure of the Silsoe cube was experimentally measured with pressure taps; thus, the present numerical model was successively validated against these measurements as discussed in the next Section. Three different cubes arrangements and the smoke fire dispersion from different diesel pool fire locations were considered as shown in Figure 1. Each column array was marked with a unique letter. All cubes were of an $H = 6$ m height and they were shifted in lines and columns of 6 m distance. For Case 1, the pool fire was placed between the D1 and D2 cubes that were in a distance $3H$ and C1 and E1 cubes that were in the distance H . For Case 2, the pool fire was placed between B2 and B3 cubes that were in distance H and A2 and C2 cubes that were in distance $3H$. Finally, for Case 3, the pool fire was placed between A and B columns. The wind flow direction in each Case is also shown in Figure 1. The smoke concentration level was studied along A, B, C, and D lines. All the lines were placed at an H distance from the center of the diesel pool fire accident.

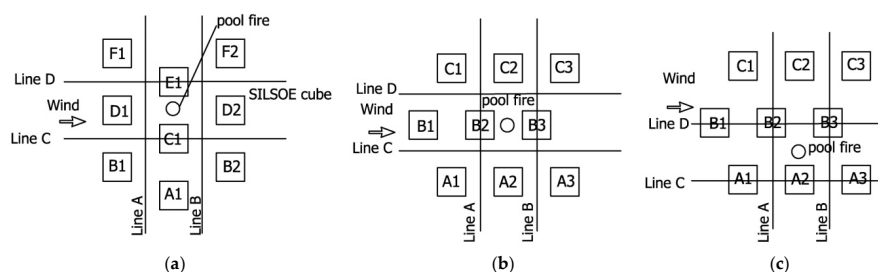


Figure 1. Model city buildings arrangement (marked squares), diesel pool fire location (circle) and wind direction (arrow) for (a) Case 1 where the Silsoe cube is also indicated; (b) Case 2; and (c) Case 3.

The computational domain was extended at $X = 20H$, $Y = 20H$, and $Z = 8H$ in the streamwise, the perpendicular, and the height direction. For each case, the diesel pool fire was set at the center of the domain as shown in Figure 1 at $X = Y = Z = 0$.

2.2. Fundamental Equations

The Fire Dynamics Simulation (FDS) is a low-speed code (the Mach number is less than 0.3) that numerically solves the Navier-Stokes equations. It was applied to thermally driven flow. The FDS model was validated against a wide variety of full scale experiments. The FDS model is a low Mach, Large eddy Simulation code. A low pass-filter was applied for the derivation of the mass, momentum, and energy equations. The Smagorinsky form of the LES models was applied to define the turbulence characteristics [47].

The LES approach develops the filtered mean values of mass, momentum, and energy and takes into account the effect of the subgrid model. A mass-weighted Favre filter was applied such as $\bar{\rho} \tilde{\varphi} \equiv \overline{\rho \varphi}$. The filtered field, denoted with a bar and with the “~” symbol, was denoted the mass-weighted mean property.

The Favre-filtered equations are:

$$\frac{\partial \bar{\rho}}{\partial t} + \frac{\partial (\bar{\rho} \tilde{u})}{\partial x_i} = 0, \quad (1)$$

$$\frac{\partial \bar{\rho} \tilde{u}}{\partial t} + \frac{\partial}{\partial x_j} (\bar{\rho} \tilde{u}_i \tilde{u}_j) = -\frac{\partial \bar{p}}{\partial x_i} - \frac{\partial \bar{\tau}_{ij}}{\partial x_j} + \bar{\rho} g_i, \quad (2)$$

where, ρ is the density, g is the gravity acceleration, u is the velocity, p is the pressure, t is the time, and $\tau_{ij} = \mu (2 S_{ij} - \frac{2}{3} \delta_{ij} (\nabla \cdot u))$ is the stress tensor.

The filter advection term is $\tilde{u}_i \tilde{u}_j = \tilde{u}_i \tilde{u}_j + \tau_{ij}^{sgs}$, where τ_{ij}^{sgs} is the subgrid scale stress (SGS). The SGS is decomposed and the Newton’s law of viscosity is applied.

The filter Navies Stokes equation is reformed as [47]:

$$\frac{\partial \bar{\rho} \tilde{u}}{\partial t} + \frac{\partial}{\partial x_j} (\bar{\rho} \tilde{u}_i \tilde{u}_j) = -\frac{\partial \bar{p}}{\partial x_i} - \frac{\partial \tau_{ij}^{dev}}{\partial x_j} + \bar{\rho} g_i \quad (3)$$

where τ_{ij}^{dev} is the total deviatoric stress and is expressed as $\tau_{ij}^{dev} = 2(\mu + \mu_t) (\bar{S}_{ij} - \frac{1}{3} (\nabla \cdot \tilde{u}) \delta_{ij})$, μ is the dynamic viscosity of the fluid, S_{ij} is the strain tensor, and δ_{ij} is the Kronecker delta.

The turbulent viscosity μ_t is modeled with the Smagorinsky analysis as:

$$\mu_t = \rho (C_s \Delta)^2 \left(2 S_{ij} S_{ij} - \frac{2}{3} (\nabla \cdot \tilde{u})^2 \right)^{1/2}, \quad (4)$$

$C_s = 0.2$ is the Smagorinsky coefficient, Δ is the filter lengthscale.

The energy conservation equation is written as:

$$\frac{\partial}{\partial t} (\bar{\rho} \tilde{h}_s) + \frac{\partial (\bar{\rho} \tilde{u}_i \tilde{h}_s)}{\partial x_i} = \frac{\partial}{\partial x_i} \left[\left(\frac{\mu}{Pr} + \frac{\mu_t}{Pr_t} \right) \frac{\partial \tilde{h}_s}{\partial x_i} \right] + \dot{q}''' + \nabla \cdot \dot{q}'', \quad (5)$$

where, h_s is the sensible enthalpy, $\dot{q}'''$ is the heat release per unit volume from the chemical reaction, $\dot{q}''$ are the radiative and conductive heat fluxes, Pr is the Prandtl number, and Pr_t is the turbulent Prandtl number with value 0.5.

The transport equation for species is written as:

$$\frac{\partial \bar{\rho} \tilde{Y}_i}{\partial t} + \frac{\partial}{\partial x_j} (\bar{\rho} \tilde{u}_j \tilde{Y}_i) = \frac{\partial}{\partial x_j} \left[\left(\rho D_i + \frac{\mu_t}{Sc_t} \right) \frac{\partial \tilde{Y}_i}{\partial x_j} \right], \quad (6)$$

where, D_i is the diffusivity of species i , Y_i is the mass fraction of species i , and Sc_t is turbulent Schmidt number with value 0.8.

2.3. Numerical Details and Validation

An explicit predictor-corrector finite difference scheme was applied. This scheme was second order accurate in time and space. In each time step, the Poisson equation for modified pressure was solved by a direct FFT-based solver. An explicit second-order Runge-Kutta scheme was applied for the flow variables which were updated in time.

The convective terms were upwind-biased differences in the predictor step and downwind biased differences in the corrector step. The material and thermal diffusion terms were central differences, with no upwind or downwind bias. The same difference was used during the predictor and corrector steps. FDS uses a structured staggered grid with the immersed boundary method (IBM) for the treatment of the flow obstruction [48].

The computational mesh is important for the accuracy of the numerical model. The characteristic grid spacing is defined from the expression [47]:

$$D^* = \left(\frac{Q}{\rho_\infty c_p T_\infty \sqrt{g}} \right)^{2/5}, \quad (7)$$

where, T_∞ is the ambient air temperature, c_p is the specific heat, ρ_∞ is the air density, g is the gravitational acceleration, and Q is the heat rate release. A uniform grid size was applied at the computational domain with a value equal to $D^* = 0.273$ m. The numbers of cells were 5,200,000, and the duration of the simulation lasts for 250 s.

During the calculation, the time step was adjusted so that the Courant–Friedrichs–Lewy (CFL) condition should be lower than 1 ($CFL < 1$). The averaging of fluid flow and transport quantities were recorded between 100 s, where the fire dispersion starts, and 250 s. The initial transient at 100 s was adequate for the flow field to become stationary. The concentration averaged at 250 s when the smoke plume was fully developed.

Results from the present simulations were compared successively against experimental data [45,46] for the pressure coefficient, C_p , defined by:

$$C_p = \frac{p_s - p_\infty}{\frac{1}{2} \rho u_\infty^2}, \quad (8)$$

where, p_s , is the local static pressure, p_∞ , is free-stream static pressure, and u_∞ is the free stream velocity. As shown in Figure 2, the present numerical results were fairly good as compared against the experimental results of the Silsoe cube.

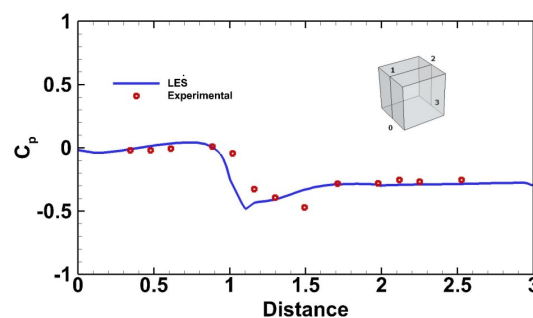


Figure 2. Pressure coefficient around the Silsoe Cube situated in the building array of Case 1, with “-” as the present results and with “o” as the measurements from the King, Gough [45] experiments.

2.4. Boundary Conditions

The Silsoe research site experimental data were applied for the inlet velocity condition [49]. The velocity at the inlet boundary condition was applied as:

$$U(z) = \frac{u_*}{\kappa} \ln\left(\frac{z + z_o}{z_o}\right), \quad (9)$$

$$u_* = \frac{\kappa U_{ref}}{\ln\left(\frac{z_{ref}}{z_o}\right)}, \quad (10)$$

where $\kappa = 0.4$ is the von Karman's constant, $z_{ref} = H$ is the reference height, $z_o = 0.01$ m is the ground roughness height [50], and the undisturbed approach of the flow velocity at the cube's height is $U_{ref} = 10.08$ m/s.

The lateral boundary conditions were set as periodic. An open boundary where the fluid is allowed exit from the computational domain was applied at the outflow condition. At the outflow boundary, the standard zero gradient condition was applied. The floor of the domain and the cube's wall were modeled with a log-law velocity profile.

2.5. Diesel Pool Fire

A fire is a reaction of a hydrocarbon fuel with oxygen that produces carbon dioxide and water vapor. Most of the time, air is inefficient, and this has as a result the production of multiple combustion products. In order to limit the computational time, a simplified approach to the chemistry was applied involving six gas species (Fuel, CO₂, CO, H₂O, O₂, N₂) and soot particles. The air, the fuel, and the fire products are referred to as 'lumped species'. Fuel and products species were explicitly computed. The lumped species approach was the accordance with the mass transport equations.

The diesel pool fire incident had a $D = 3$ m diameter. The incident had the same characteristics of the Chatris, Quintela [31] experimental study with different geometry and wind flow conditions. The fuel mass loss rate $\dot{m}''$ and the total heat release rate $\dot{q}$ (HRR) were defined by the following equations [51]:

$$\dot{m}'' = \dot{m}''_{\infty} \left(1 - e^{-k \beta D}\right), \quad (11)$$

$$\dot{q} = \dot{m}'' \Delta H_{c,eff} A_f, \quad (12)$$

where, $\dot{m}''_{\infty}$ is the infinite-diameter pool mass-loss rate, $\Delta H_{c,eff}$ is the heat of combustion, A_f is the surface area of the pool, β is the "mean beam length corrector", and k is the absorption extinction coefficient of the flame.

According to the experimental results, the mass burning rate for a diesel pool fire with a 3 m diameter is about $0.045 \frac{\text{kg}}{\text{sec m}^2}$ and the total heat release rate $\dot{q}$ (HRR) is 13.5 MWatt.

Another important parameter in order to define the smoke products is the smoke yield. The smoke yield is defined as the amount of burned fuel (kg smoke/kg fuel). Walton et al. [52] assumed that the smoke yield from a diesel fire varies between 15% and 20%; Argyropoulos [33] proposed an average 17.5% for the smoke yield. In our study, the smoke yield is defined as 17.5%.

Assael and Kakosimos [53] defined the risk zones where the toxic concentration could place the human's health in danger. A risk zone is a circular area which has as a center at the point of the source emission, and is extended to the limit where safety is ensured. Risk zones cover incidents of heat flux and toxic substance in case of fires. Different zones are defined:

- Zone I—Very Serious Consequences, Lethal Concentration 50% (LC50 region). The possibility of death population in this zone is 50% due to inhalation of a toxic substance.
- Zone II—Serious Consequences, Lethal Concentration 1% (LC1 region). The possibility of death population in this zone is 1% due to inhalation of a toxic substance.
- Zone III—Moderate Consequences, Immediately Dangerous to Life and Health (IDLH region). Zone III could lead to reversible injuries following the inhalation of a toxic substance. Outside the Zone III is the safe area.

The values of the safety limits of the fire smoke pollutants are defined from the National Institute for Occupational Safety and Health (NIOSH) as $LC1 = 25,000 \text{ (mg/m}^3\text{)}$ and $IDLH = 2500 \text{ (mg/m}^3\text{)}$.

3. Results and Discussion

3.1. Flow Field Results

The FDS code performs large eddy Simulations analysis for a diesel pool fire accident inside an array of cubes. The mean flow in the staggered cubes array is very complicated as it is characterized by different vortices as shown in the streamlines of Figure 3. It is detached on the roof top of the buildings and forms vortices simultaneously with the side vortices that are also formed at the buildings. These vortices enter inside the street intersections and influence the flow characteristics inside the cubes' rows and columns. Important helicoid vortices are formed behind the buildings of the first column which are responsible for the fire's products dispersion. This phenomenon is decreasing in the second column of the array, and finally, wake vortices are formed behind the last column of the cubes.

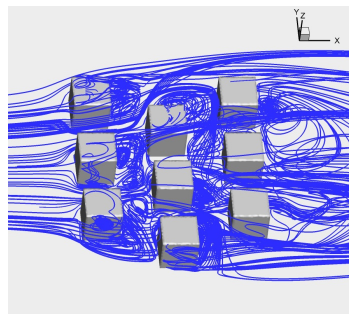


Figure 3. Prospective streamline plot of the mean flow in the array of cubes of Case 1.

In Case 1, the cube lines were staggered perpendicular of the wind direction which means that the wind did not flow symmetrically. As shown in Figure 4a for the streamlines at the plane $Z = 1 \text{ m}$, the asymmetry had an important effect to the flow distribution. Two recirculations behind the D1 cube and a smaller one at the lateral face appeared. The streamlines diverged between the C1 and E1 cubes, at the pool fire incidence location. A smaller lateral recirculation appeared at the lateral face of the C1 cube. In contrast, Case 2 led to a more symmetrical flow. As shown in Figure 4b, similar mirror recirculations appeared at the fire symmetry axis, $Y = 0$, while the streamlines at the fire position reversed towards the Cube B2. Finally, the streamlines of Case 3 are presented in Figure 4c. It was found that the pool fire location was not affected by the cube's recirculation zone. The buoyancy forces were so strong that an important asymmetry was found and a major horizontal recirculation zone formed inside the street canyon.

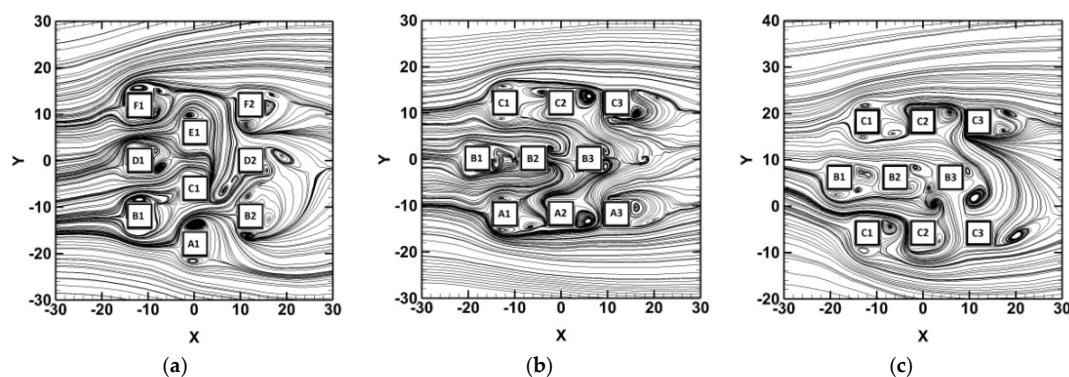


Figure 4. Time-averaged streamlines of the horizontal plane $Z = 1 \text{ m}$ for (a) Case 1; (b) Case 2; (c) Case 3.

Figure 5a–c present the time-average streamlines for the fire symmetry plane at $Y = 0$ m for the Cases 1, 2 and 3, respectively. From this figure, it is shown that the buoyancy-driven forces due to the fire are relatively stronger in the vertical direction than the wind inertia forces. This phenomenon leads the smoke dispersion patterns outside the cube's array.

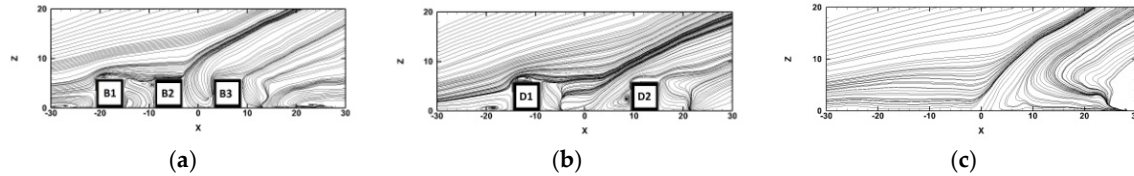


Figure 5. Time-averaged streamlines at the symmetry plane $Y = 0$ m for (a) Case 1; (b) Case 2; (c) Case 3.

Figure 6 shows the smoke dispersion snapshots of the diesel pool fire after 200 s of the incidence for the three studied cases. The general observation is that the smoke plume was driven by the buoyancy forces and the wind flow, and reached at the top of the cube's arrays. Due to the importance of the buoyancy forces, the smoke was moved outside the arrays, and only a small part of it recirculated between the cubes.

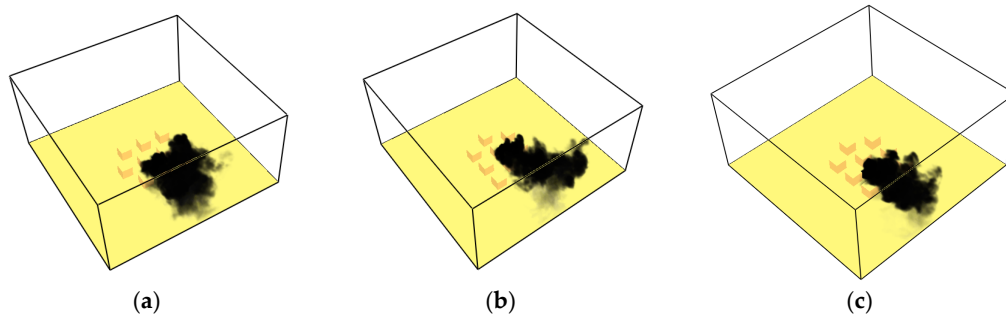


Figure 6. Snapshots of the dispersion of smoke after 200 s of the incidence for (a) Case 1; (b) Case 2; (c) Case 3.

The identification of vortices and coherent structures could be made with the iso-surfaces of the Q-criterion. The Q-criterion is defined as:

$$Q = C_Q (\Omega^2 - S^2), \quad (13)$$

where, C_Q is a constant for the impressions, $S_{ij} = \frac{1}{2} \left(\frac{\partial u_j}{\partial x_i} + \frac{\partial u_i}{\partial x_j} \right)$ is the strain rate, and $\Omega_{ij} = \frac{1}{2} \left(\frac{\partial u_j}{\partial x_i} - \frac{\partial u_i}{\partial x_j} \right)$ is the vorticity rate tensors.

In Figure 7 the $Q = 0.1$ level was selected to better visualize the turbulent structures for the three different cases. It can be seen that the horseshoe vortex formed on the leeward face of all the cubes that are in the direction of the induced wind. Hairpin vortices are formed for all array cubes of Case 1, while for Case 2 and 3, hairpin vortices formed only for the first line of the array cubes that faced the incoming wind. The pool fire source for Case 1 and 2 was located in the wake zone of D1 and B2 cubes, respectively. The flow inside these wake zones formed a strong mixing and turbulence generation region. As shown in Figure 7, a fire accident produced important coherent structures that exceeded the cubes array height.

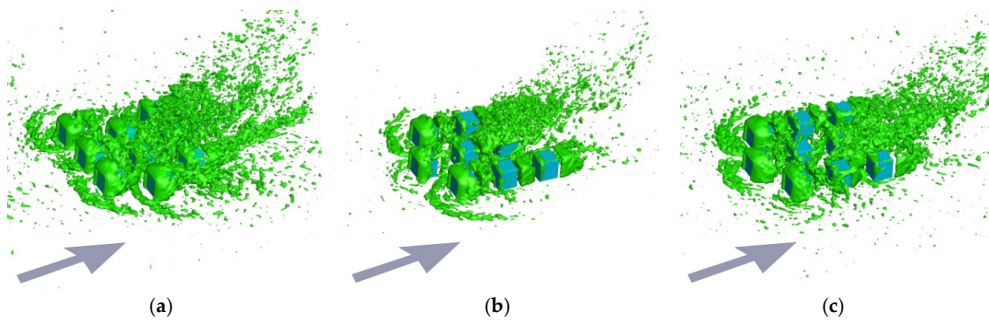


Figure 7. Snapshots of the Q criteria for (a) Case 1; (b) Case 2; (c) Case 3.

3.2. Smoke Concentration

Figures 8–10 show the average smoke concentration along A, B, C and D lines for Case 1, Case 2 and Case 3, respectively. As shown in Figure 8a, the smoke concentration leeward the fire position (A line) is negligible.

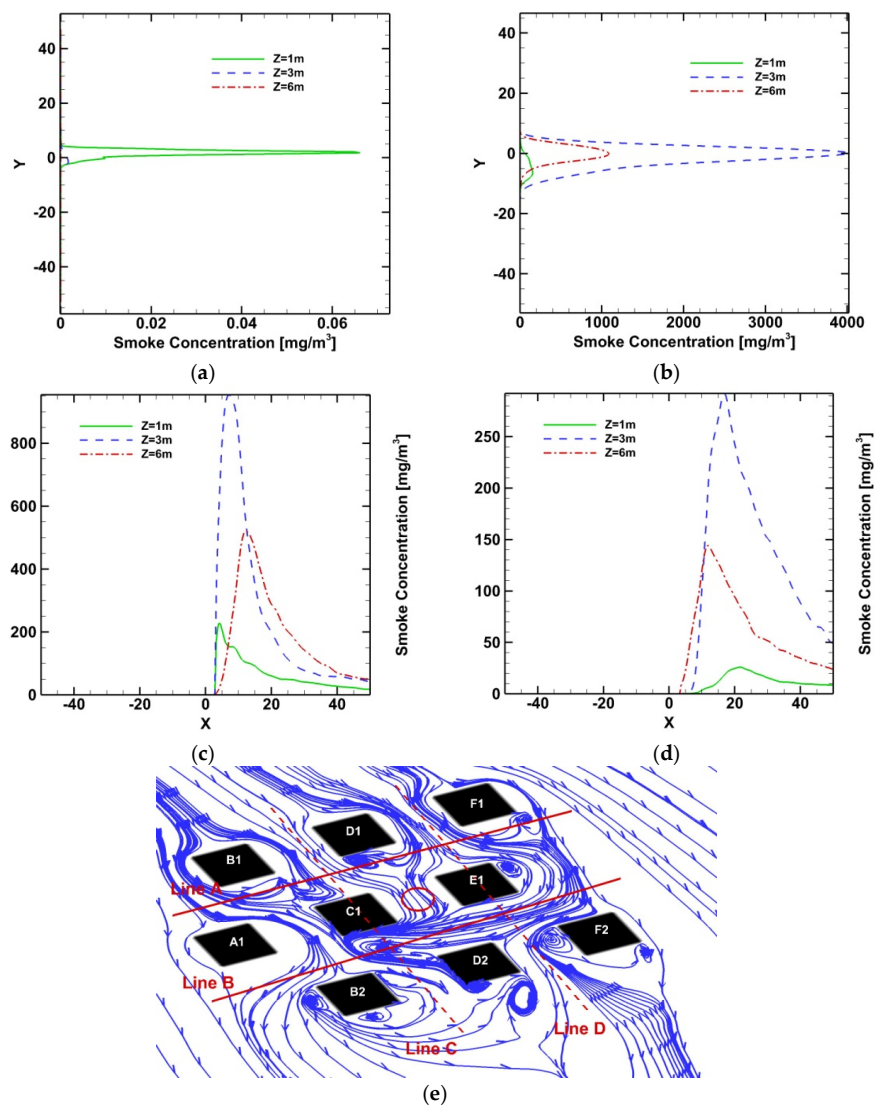


Figure 8. Smoke average concentration distribution along (a) line A; (b) line B; (c) line C; (d) line D for Case 1 and (e) the streamlines that define it.

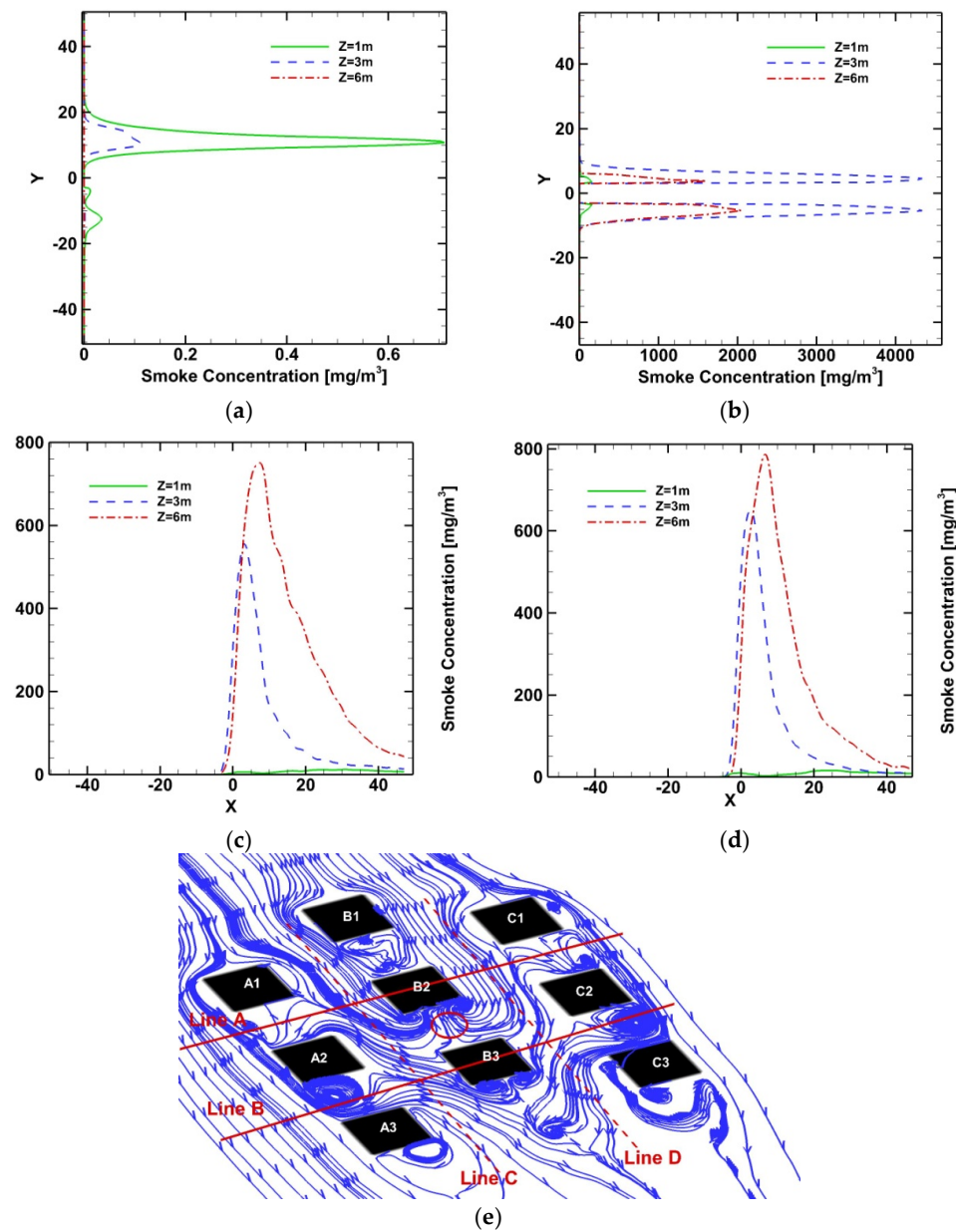


Figure 9. Smoke average concentration distribution along (a) A line; (b) B line; (c) C line; (d) D line for Case 2 and (e) the streamlines that define it.

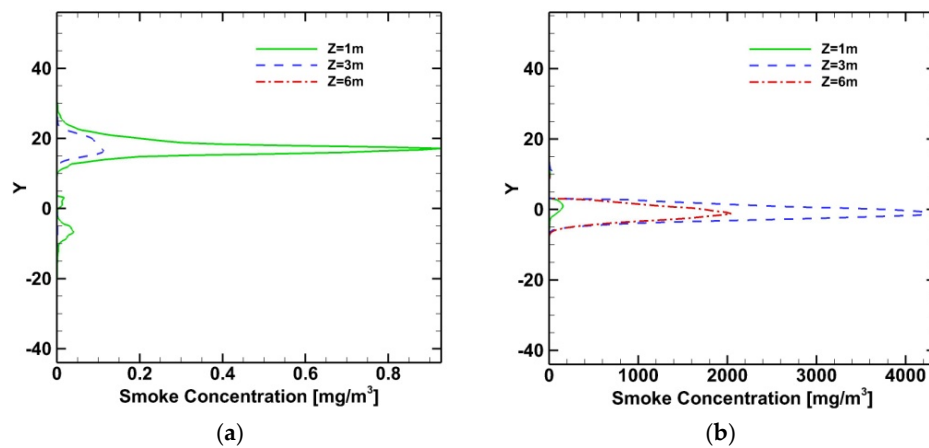


Figure 10. Cont.

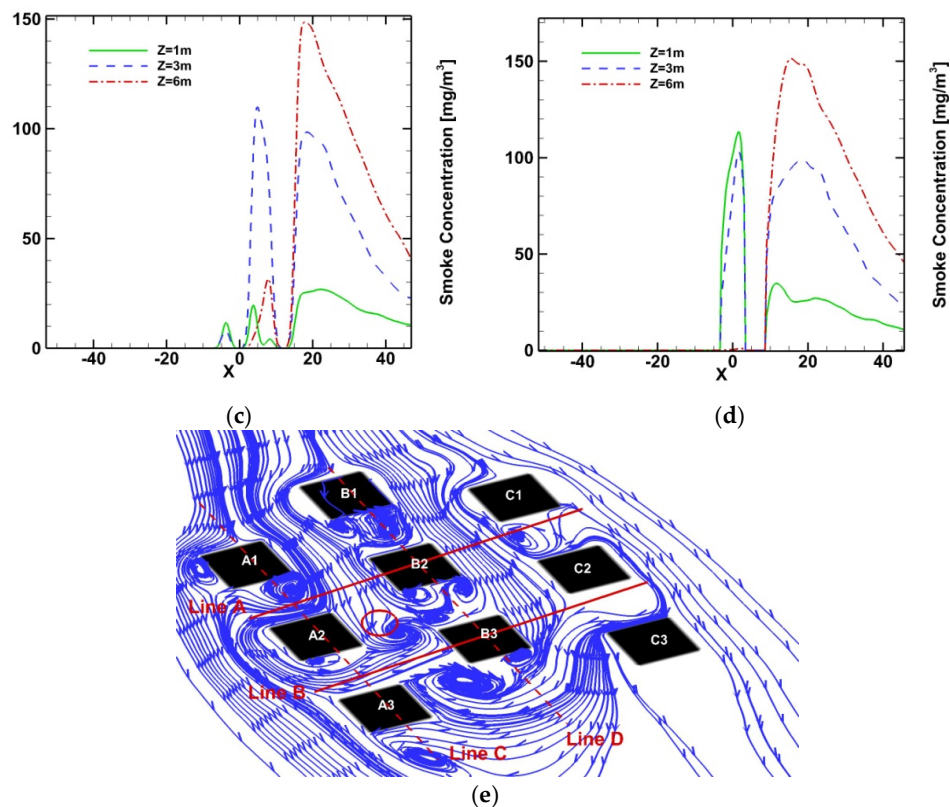


Figure 10. Smoke average concentration distribution along (a) line A; (b) line B; (c) line C; (d) D line for Case 2 and (e) the streamlines that define it.

As shown from the streamlines on Figure 8e, the smoke was channeled along line B. Additionally, an important recirculation zone was created leeward of the C1 cube, which trapped the smoke. In this region, the smoke concentration reached its highest limits. Additionally, the smoke concentration had higher values at the $Z = 3\text{ m}$ level (Figure 8b). Along line C (Figure 8c) the smoke concentration was more important than this of line D (Figure 8d).

Figure 9a shows that the smoke concentration at the windward line A of the fire position was minimum; however, it presented slightly higher values than in Case 1. Figure 9b shows that the maximum values of smoke concentration were presented at the lateral sides of the B3 cube. As shown in Figure 9c,d, the smoke concentration distribution was quite similar for both C and D lines. This is due to the symmetry of the flow and the pool's fire position.

Finally, in Figure 10a, the smoke concentration at the leeward line A of the fire position was also minimum. Along line B (Figure 10b), the smoke concentration distribution was at its maximum level at 3 m height. Along lines C and D, the smoke concentration was changing with complex variations due to complex flow phenomena caused by the cubes' blockage. In Figure 10c, the smoke concentration between A1 and A2 presented the highest values at the $Z = 3\text{ m}$ height. Between A2 and A3 cubes, the highest values of concentration were at the $Z = 6\text{ m}$ height. In Figure 10d the smoke concentration between B1 and B2 cubes was maximum at $Z = 1\text{ m}$ height. Between B2 and B3 cubes, the maximum level was at $Z = 6\text{ m}$ height.

3.3. Safety Limits

For firefighting measures, it is important to define the safety limits between the urban building blocks. The directives of the National Institute for Occupational Safety and Health (NIOSH) in the USA define the safety limits for the fire pollutants (smoke, CO and SO_2 etc.). The safety limits of the LC1 Zone for the smoke concentration is $25,000\text{ mg/m}^3$, and for the IDLH Zone is 2500 mg/m^3 . The limits

of the IDLH zones with contour graphs give practical visual information for the danger zones and the definition of the intervention zones.

Figures 11 and 12 present the limits of the LC1 and IDLH zones for the three different cases after 200 s at the fire's symmetry plane and a horizontal plane placed $Z = 1$ m above the ground. The LC1 zone is indicated with the red color and the IDLH zone with the green color.

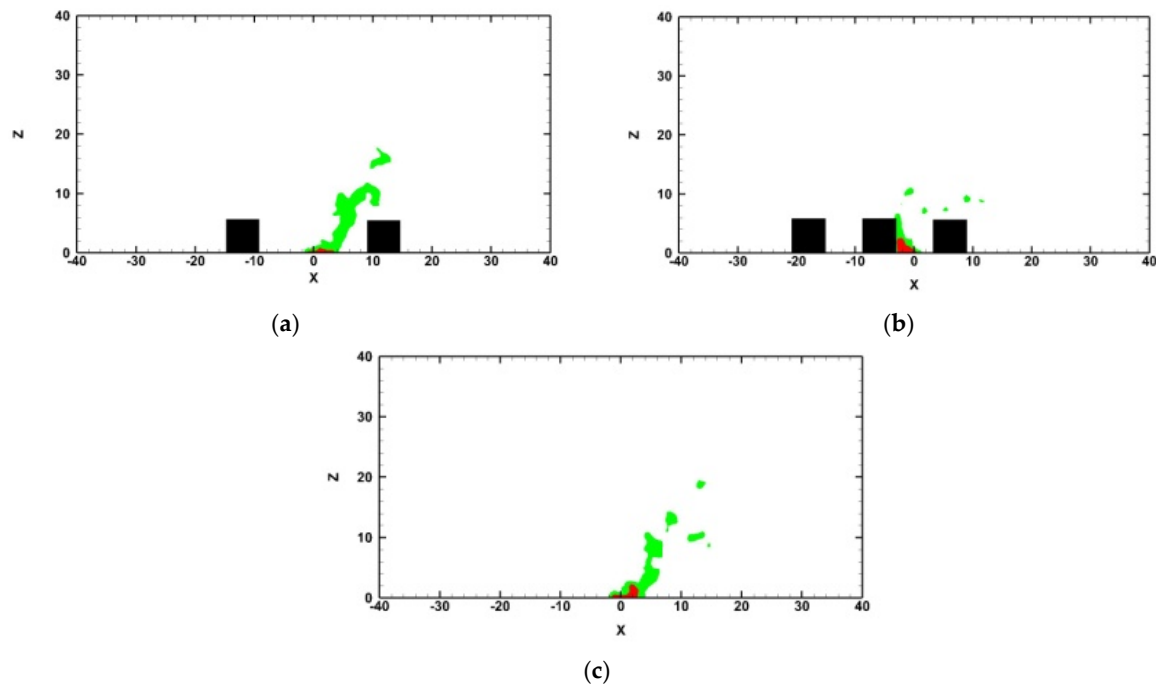


Figure 11. The LC1 zone and the IDLH zone at the fire's symmetry for (a) Case 1; (b) Case 2; (c) Case 3 after 200 s of the fire incidence at the.

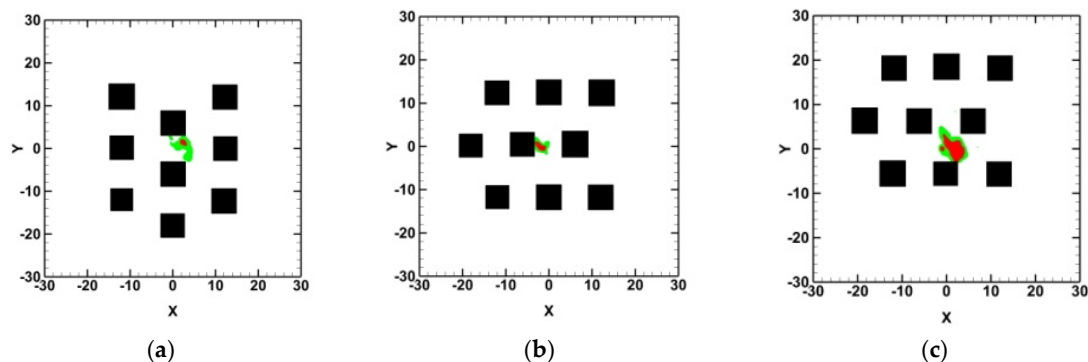


Figure 12. The LC1 and IDLH zones for a horizontal plane at $Z = 1$ m above the ground for (a) Case 1; (b) Case 2; (c) Case 3, after 200 s of the fire accident.

As is shown in Figures 11a and 12a, the IDLH smoke zone dispersed towards the D2 cube. For this reason, all the cube's façade openings of this side should be closed and protected in a street fire case. Most of the smoke products exited the street canyon before reaching the D2 cube. A wider distribution of the IDLH zone was presented between the C1 and E1 cubes. The non-symmetrical geometry had as an effect a wider distribution of the IDLH zone between the cubes. According to Figures 11b and 12b, the IDLH smoke zone dispersed towards the leeward facade of the B2 cube. All the cube's façade openings at this side should be closed and protected in a street fire case. Finally, Figures 11c and 12c present the IDLH smoke zone from a fire incident that was not placed in a cube's recirculation zone. The tilt of the IDLH smoke zone escaping the cube's arrays height was similar for all the cases.

Table 1 defines the zone limits of the LC1 and IDLH zones for all the studied cases and for the Fire's symmetry plane and a Horizontal Plane at $Z = 1$ m above the ground. Case 2 presents the most extended area of the LC1 zone (4.2 m) at the Horizontal plane $Z = 1$ m. Both Case 1 (1.35 m) and Case 3 (1.8 m) presented a similar LC1 zone extension. At the same plane, Case 3 presented the most extended area of the IDLH zone (5.83 m), and Case 1 (4.2 m) came after. At the fire's symmetry plane, Case 3 presented the higher limits for both LC1 (2.5 m) and IDLH (23.32 m) zones. Concerning the LC1 zone, Case 1 presented the smallest radius extension of the 0.6 m radius, and Case 2 presented a 1.96 m radius extension. Finally, Case 1 presented an important IDLH radius extension of 18.5 m, and Case 2 presented a 10.4 m extension.

Table 1. LC1 and IDLH radius for Case 1, 2, and 3.

	Case 1	Case 1 (Radius)	Case 2 (Radius)	Case 3 (Radius)
LC1 zone	Horizontal Plane $Z = 1$ m	1.35 m	4.2 m	1.8 m
IDLH zone	Horizontal Plane $Z = 1$ m	4.2 m	2.46 m	5.83 m
LC1 zone	Fire's symmetry plane	0.6 m	1.96 m	2.5 m
IDLH zone	Fire's symmetry plane	18.5 m	10.4 m	23.32 m

4. Conclusions

This study examined how a diesel pool fire incident affected the wind flow in a staggered array of cubes. The different urban geometry determined the wind distribution and the smoke dispersion. Several predictions for the smoke dispersion and the fire accident position could be made for an urban area. Additionally, it defined the IDLH smoke zones for an incident occurring in a complex urban morphology and proposed the measurements for a quick response estimating the immediate intervention. The limits of the IDLH zones with contour graphs gave practical visual information for the danger zones and the definition of the intervention zones.

For a small distance between buildings and a perpendicular wind applied, a fire accident will direct the smoke towards the windward building. In a symmetrical geometry of urban blocks, the smoke after a fire accident will also be symmetrically dispersed. If the fire was between two buildings with a long distance, the smoke will be driven towards the leeward building. Complex geometries without any axis of symmetry could lead to unpredictable flows due to the fact that the wind may prefer to follow a specific path that could not be predicted with pre-planned actions. Finally, if the fire was placed in a road and the wind is parallel during the accident, the smoke followed the wind direction but was disturbed from the building's lateral recirculation's.

The LC1 and IDLH zone limits were calculated for all the cases. Street canyons, such as in Case 2, with small street width to building's height ratio, presented the highest LC1 limits for the horizontal planes at 1 m height from the ground level. A pool fire that was placed in a well-ventilated position without a trap for the smoke pollutant presented an important extension of the IDLH zone along the wind direction.

Different wind velocities should be studied in order to define the possibility of the smoke re-entering back into the array's cubes.

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