

From post-combustion carbon capture to sorption-enhanced hydrogen production: A state-of-the-art review of carbonate looping process feasibility

Dawid P. Hanak*, Sebastian Michalski, Vasilije Manovic

Clean Power Engineering, Energy and Power, School of Water, Energy and Environment, Cranfield University, Bedford, Bedfordshire MK43 0AL, UK



ARTICLE INFO

Keywords:

Calcium looping
Hydrogen production
Techno-economic assessment
Clean technologies
Clean energy
Efficiency improvement

ABSTRACT

Carbon capture and storage is expected to play a pivotal role in achieving the emission reduction targets established by the Paris Agreement. However, the most mature technologies have been shown to reduce the net efficiency of fossil fuel-fired power plants by at least 7% points, increasing the electricity cost. Carbonate looping is a technology that may reduce these efficiency and economic penalties. Its maturity has increased significantly over the past twenty years, mostly due to development of novel process configurations and sorbents for improved process performance. This review provides a comprehensive overview of the calcium looping concepts and statistically evaluates their techno-economic feasibility. It has been shown that the most commonly reported figures for the efficiency penalty associated with calcium looping retrofits were between 6 and 8% points. Furthermore, the calcium-looping-based coal-fired power plants and sorption-enhanced hydrogen production systems integrated with combined cycles and/or fuel cells have been shown to achieve net efficiencies as high as 40% and 50–60%, respectively. Importantly, the performance of both retrofit and greenfield scenarios can be further improved by increasing the degree of heat integration, as well as using advanced power cycles and enhanced sorbents. The assessment of the economic feasibility of calcium looping concepts has indicated that the cost of carbon dioxide avoided will be between 10 and 30 € per tonne of carbon dioxide and 10–50 € per tonne of carbon dioxide in the retrofit and greenfield scenarios, respectively. However, limited economic data have been presented in the current literature for the thermodynamic performance of calcium looping concepts.

1. Introduction

Decarbonisation of the power sector, which is responsible for a third of the anthropogenic greenhouse gas (GHG) emissions [1], is critical to meeting the targets established by the Paris Agreement that recommended keeping the global mean temperature increase below 2 °C and undertaking efforts to limit it to 1.5 °C above pre-industrial levels to significantly reduce the risks and impacts of climate change [2]. Transformation of this sector is essential to meet both environmental and energy demand targets, while ensuring sustainable utilisation of natural resources and keeping the cost of electricity at an affordable level. Despite the potential improvements in their efficiency, unabated conventional fossil fuel-fired power generation systems are not able to meet these environmental targets. As there are no other technologies

that could significantly reduce emissions from fossil fuel-fired power generation systems, which are expected to remain in the electricity mix for the foreseeable future, carbon capture and storage (CCS) is seen as crucial to decarbonising the power sector [3]. Importantly, the 2DS scenario assumes that CCS will contribute to nearly 14% reduction in global carbon dioxide (CO₂) emissions by 2050 [4]. It has also been estimated that the exclusion of CCS may increase the cost of achieving emission reduction targets by up to 70% [5].

Although considerable progress has been made in reducing the energy intensity of mature CO₂ capture and separation technologies, these are still expected to reduce the net efficiency of the reference power generation system by at least 7% points [6,7]. This corresponds to at least 60% increase in the electricity cost [8], hindering the deployment of CCS in the power sector. It also needs to be highlighted that such a

Abbreviations: 2DS, 2°C scenario; AC, cost of CO₂ avoided; ASU, air separation unit; CaL, carbonate looping; CaLC, carbonate looping combustion; CCS, carbon capture and storage; CCU, CO₂ compression unit; CFPP, coal-fired power plant; CPU, CO₂ purification and compression unit; GHG, greenhouse gas; HEN, heat exchanger networks; IGCC, integrated-gasification combined cycle power plant; IGFC, integrated-gasification fuel cell; NGCC, natural gas combined cycle power plant; LCOE, levelised cost of electricity; SESR, sorption-enhanced steam reforming process; SEWGS, sorption-enhanced water-gas shift; SOFC, solid-oxide fuel cell; ZECOMAG, zero-emissions coal mixed technology with air gas turbine; ZECOMIX, zero-emissions coal mixed technology

* Corresponding author.

E-mail address: d.p.hanak@cranfield.ac.uk (D.P. Hanak).

<https://doi.org/10.1016/j.enconman.2018.09.058>

Received 24 April 2018; Received in revised form 13 September 2018; Accepted 18 September 2018

0196-8904/ © 2018 The Authors. Published by Elsevier Ltd. This is an open access article under the CC BY license (<http://creativecommons.org/licenses/by/4.0/>).

Nomenclature

Subscripts

el	electrical energy
th	thermal energy
gross	value based on gross power output
vol	value on volumetric basis

reduction in the net efficiency was found to impose the largest impact on the environmental performance of mature CO₂ capture and separation technologies, as it will result in increased fuel consumption to achieve the same net power output. In turn, it will affect the upstream processes associated with extraction, preparation and transportation of fuels [9]. As a result, CCS is predicted to result in 64% [10] to 80% [11] reduction of GHG emissions over the entire system lifetime even though it is commonly designed to remove 90% of CO₂ from combustion of fossil fuels [10]. Therefore, less energy-intensive technologies, such as high-temperature solid looping cycles, are currently being developed [12]. Carbonate looping (CaL), which is based on the reversible carbonation reaction of CO₂ with a metal oxide, such as calcium oxide (CaO) or magnesium oxide (MgO), is regarded as an emerging technology for decarbonisation of fossil fuel power generation systems [6]. This is because it has been shown not only to reduce the efficiency penalties, but also to increase the net power output of the retrofitted system [7]. The main reason behind such improvement, when compared to the mature CO₂ capture and separation technologies, is the high-temperature operation of CaL, enabling high-grade heat to be recovered, as well as clean and efficient syngas generation.

Application of CaL for decarbonisation of fossil fuel-fired power generation systems was first proposed two decades ago by HIRAMA et al. [13] and Shimizu et al. [14]. Since then, this concept has been

developed via both experimental testing and thermodynamic modelling [7]. It needs to be highlighted that significant developments have been achieved after 2009 that led to demonstration of CaL at the megawatt scale: the 1 MW_{th} unit in Darmstadt [15], the 1.7 MW_{th} unit in Oviedo (La Pereda) [16], and the 1.9 MW_{th} unit at the Industrial Technology Research Institute (ITRI), Taiwan [17]. The development of CaL has been regularly reviewed with respect to a range of progress activities as summarised in Table 1. These focused on the experimental and pilot plant testing activities [7,18,19], sorbent performance and development [6,18–27], process modelling [7,25,28,29], and CaL configurations for fossil fuel-fired power plants [7,20,28] and hydrogen production [19]. As can be seen in Table 1, the recent studies focused mostly on developments in CaL retrofits to existing fossil fuel-fired power generation systems, rather than on novel greenfield power plants utilising CaL-based combustion and sorption-enhanced hydrogen (H₂) production processes. Moreover, emphasis was put on improvements from the process thermodynamics and sorbent development standpoints. It is crucial, however, to understand whether such performance improvements are substantiated by the improvements in the economic performance that will support commercial deployment of CaL. Therefore, to build on the previous reviews in this field, this work aims to guide further development of the high-efficiency low-emission fossil fuel-fired power generation and hydrogen production systems based on CaL by:

- comprehensively reviewing progress in the development of CaL concepts for retrofitting conventional fossil fuel-fired power generation systems;
- providing a comprehensive overview of greenfield power generation concepts based on CaL combustion and sorption-enhanced hydrogen production processes; and
- conducting a statistical evaluation of the techno-economic feasibility of CaL concepts using data available in the current literature.

Table 1
Summary of review studies related to the carbonate looping process.

Source	Publication date	Review scope
Stanmore and Gilot [27]	2005	<ul style="list-style-type: none"> • Summary of the sintering, sulphation, particle fragmentation and attrition effect on sorbent activity • Detailed information on the correlations for mathematical modelling of carbonation, calcination, sulphation and sintering • A brief overview of the models for prediction of the aerodynamics and trajectories of particles, as well as reaction rates in the circulating fluidised bed
Harrison [21]	2008	<ul style="list-style-type: none"> • Comparison of the standard steam-methane reforming process and the CaL process for hydrogen production • Review of the thermodynamic analyses, sorbent durability and process configurations • Review of the experimental studies on hydrogen production
Florin and Harris [19]	2008	<ul style="list-style-type: none"> • Review of process configurations for enhanced hydrogen production from biomass gasification • Summary of sorbent regeneration measures • A brief reference to sorbent activity decay
Blamey et al. [25]	2010	<ul style="list-style-type: none"> • Review of experimental trials on hydrogen production from carbonaceous fuels using carbonate looping • Detailed description of the carbonation, calcination, sintering and sorbent performance under repeated cycle operation • Summary of sorbent deactivation and reactivation measures • Review of the carbonate looping process applications
Dean et al. [18]	2011	<ul style="list-style-type: none"> • A brief summary of semi-empirical correlations allowing estimation of the sorbent conversion • Summary of carbonate looping cycle fundamentals, sorbent deactivation and sorbent performance • Review of the carbonate looping thermodynamic and economic performance, as well as its applicability in the cement industry and to hydrogen production • A brief reference to sorbent activity decay
Anthony [26]	2011	<ul style="list-style-type: none"> • Review of the pilot plant trials for CaL • Review of sorbent performance improvements and reactivation strategies for natural and synthetic sorbents
Liu et al. [24]	2012	<ul style="list-style-type: none"> • Brief outline of carbonate looping process applicability and experimental facilities • Review of sorbent performance enhancements • Review of synthesis methods for sintering-resistant sorbents
Kierzkowska et al. [23]	2013	<ul style="list-style-type: none"> • Summary of the carbonation reaction fundamentals • Review of recent developments in synthesis of CaO-based sorbents
Romano et al. [28]	2013	<ul style="list-style-type: none"> • Review of CaL process simulations and notes on further modelling activities
Boot-Handford et al. [6]	2014	<ul style="list-style-type: none"> • Summary of process performance, sorbent deactivation and regeneration • An update on CaL pilot-plant trials
Hanak et al. [7]	2015	<ul style="list-style-type: none"> • Review of test facilities worldwide and testing activities • Review of the modelling approaches • Review of CaL process configurations for improved process integration

(continued on next page)

Table 1 (continued)

Source	Publication date	Review scope
Martinez et al. [29]	2016	<ul style="list-style-type: none"> • Review of the modelling activities worldwide • Indication of research needs for further development of CaL
Perejon et al. [20]	2016	<ul style="list-style-type: none"> • Review of multicyclic sorbent behaviour • Role of energy integration and sorbent behaviour on process efficiency
Erans et al. [22]	2016	<ul style="list-style-type: none"> • Review of techniques to enhance natural sorbent performance and to synthesise new sorbents • Review of measures to reactivate and reuse deactivated sorbent

2. Carbonate looping process

Since being patented in 1933, development of CaL has mainly focused on sorption-enhanced hydrogen production [21] and CO₂ capture from fossil fuel-fired power generation systems [14]. In both applications, the most commonly considered process configuration comprises two interconnected circulating fluidised beds (Fig. 1) that, when linked with a heat exchanger network, is characterised with thermal efficiency similar to that of current combustion systems [30]. Therefore, as opposed to other CCS technologies, high-temperature operation of CaL allows high-grade heat to be utilised in the secondary power cycle for additional power generation. If CaL was retrofitted to an existing fossil fuel-fired power generation system, the net power output of the entire process was shown to increase by more than 50% [31].

In the first reactor, the so-called carbonator, CO₂ is removed from flue gas or syngas on contact with metal oxide (Me_xO), which has been previously calcined in the calciner, via an exothermic solid-gas reaction. The carbonation process takes place at an elevated temperature, which varies between 450 °C (magnesium-based sorbents [32]) and 700 °C (calcium-based sorbents [33]), depending on the sorbent used in CaL and the partial pressure of CO₂ entering the carbonator. Under such conditions, CO₂ is removed from syngas or flue gas as metal carbonate (Me_xCO₃) at a reasonably high rate. Importantly, the carbonation process will only take place below the temperature corresponding to the equilibrium partial pressure of CO₂ in the syngas or flue gas [34]. The metal carbonate is then regenerated in another reactor, the so-called calciner, and CO₂ is reclaimed [35]. Again, the temperature at which the calcination takes place depends on the CO₂ partial pressure and type of sorbent fed to the calciner. In pure CO₂ at atmospheric pressure, this varies between 550 °C for magnesite and dolomite (partial calcination) [32], to 900 °C for dolomite (complete calcination) and limestone [33]. Under such operating conditions, a pure CO₂ stream can be theoretically achieved. Although higher operating temperatures would favour reaction kinetics, these would lead to enhanced sorbent sintering and, thus, deterioration of its CO₂ capture capacity. Importantly, the calciner can be operated at lower temperatures if steam, which can be easily separated by condensation from the CO₂ stream, is injected as a diluent. A reduction in the sorbent CO₂ carrying capacity on cycling operation as a result of sintering, attrition and sulphation is regarded as the major challenge of CaL. To maintain acceptable sorbent conversion in the carbonator, the spent sorbent needs to be partially replaced by fresh sorbent [18].

In the conventional configuration of CaL (Fig. 1), an additional amount of fuel is combusted in an oxygen/carbon dioxide (O₂/CO₂) environment to maintain the desired operating temperature in the calciner and produce a high-purity CO₂ stream. Therefore, the power required to drive the air separation unit (ASU), in addition to the CO₂ compression unit (CCU), is the main source of the parasitic load in CaL. Further reduction in the efficiency penalty associated with this technology can be achieved by reducing, or even avoiding, the need for oxygen production in the energy-intensive ASU [36]. Alternative options to provide heat for sorbent regeneration include chemical looping [37–40], which uses oxygen carriers to transfer oxygen from an air reactor to the calciner, and indirect heat transfer from a combustor via

solid heat carriers [41,42], heat transfer wall [42,43] or heat pipes [44,45].

3. Retrofits to conventional power generation systems

The existing fossil fuel-fired power generation capacity is highly dependent upon coal. However, this trend has begun to change recently and natural gas combined cycle (NGCC) power plants are expected to play an essential role in the future energy portfolio. This is mostly because of their capability for rapid changes in the operating load that will be essential to balance the energy supply and demand in the energy market with a large share of intermittent renewable energy sources [46]. Although NGCCs are characterised by lower specific CO₂ emissions compared to coal-fired power plants (CFPPs), they still need to be decarbonised for the emission reduction targets to be met by 2050. Having been considered for sorption-enhanced hydrogen production since 1933 [21], application of CaL for CO₂ capture from fossil fuel power plants was proposed for the first time by Shimizu et al. [14] in 1999. Since then, a number of CaL concepts have been proposed for decarbonisation of both CFPPs (Section 3.1) and NGCCs (Section 3.2).

3.1. Coal-fired power plants

Shimizu et al. [14] were the first to evaluate the feasibility of a CaL retrofit to a supercritical CFPP. The high-grade heat available in CaL was used to produce superheated and reheated steam at subcritical conditions. Overall, the net efficiency of the retrofitted system was estimated to be 33.4%. This was 1.4% points higher than for an oxy-fired combustor with a primary steam cycle of the same gross power output

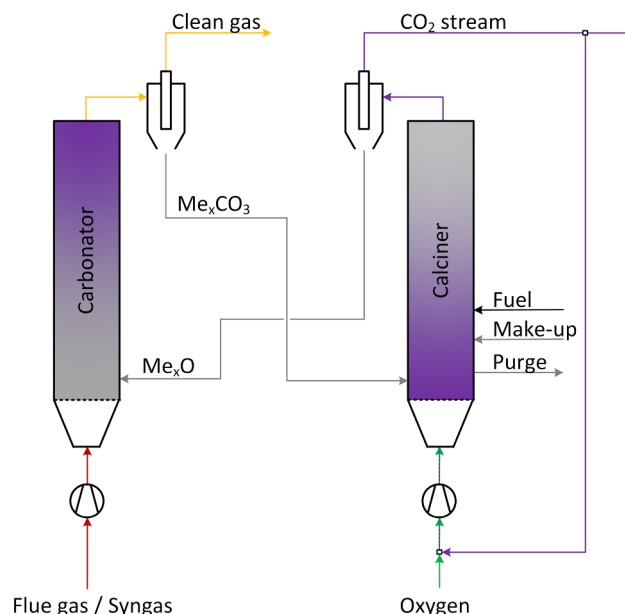


Fig. 1. Operating principle of carbonate looping for carbon capture.

and, thus, indicated the feasibility of the CaL process for reducing CO₂ emissions from CFPPs. Although this study did not provide a direct benchmark of the CaL retrofit to the reference CFPP, it stimulated other researchers to further evaluate the feasibility of such systems.

Romeo et al. [47] have investigated the retrofit of CaL to a 450 MW_{el} supercritical CFPP. Importantly, this study assumed that, in contrast to oxy-fuel combustion systems, no CO₂ recirculation was needed to control the temperature in the calciner because of the large solid inflow at 650 °C and the endothermic character of the calcination reaction. A detailed evaluation of the process configuration revealed that there were five heat integration zones that could utilise the high-grade heat from the carbonator and process streams to generate high-pressure steam and preheat the feedwater in the secondary steam cycle. Although this increased the net power output of the integrated system by 45.3%, the net efficiency dropped by 7.9% points, from 44.9% for the reference CFPP. The feasibility of the concept of CaL with no CO₂ recirculation has been confirmed by Hanak et al. [48]. The thermodynamic assessment of CaL retrofitted to the 580 MW_{el} supercritical CFPP revealed that the efficiency penalty was not affected by the level of CO₂ recirculation and was estimated to be 7.5% points. This is because, on reduction of the CO₂ recirculation from 52.8%, which corresponded to the oxygen concentration in the gas stream entering the calciner of 30%_{vol}, to zero, the net power output of the entire system and the total coal consumption were found to be reduced at the same level. Furthermore, the feasibility of the CaL retrofit to CFPPs was confirmed by Hawthorne et al. [49], Strohle et al. [50,51] and Lasheras et al. [52] who evaluated the CaL retrofits to an 1100 MW_{el} supercritical CFPP. Upon the CaL retrofit the net efficiency of the entire system was reduced by 6.3% points, from 45.6% for the reference CFPP, while the net power output increased by 45.7% [49]. Importantly, the studies by Strohle et al. [50,51] and Lasheras et al. [52] revealed that the efficiency penalty associated with CaL without CCU amounted to 2.7–3.2% points that mainly stem from the requirement for oxygen separation in the cryogenic ASU. It needs to be noted that the lower efficiency penalties reported in these studies resulted from the secondary steam cycle being operated under supercritical conditions, as opposed to the sub-critical conditions considered by Romeo et al. [47]. In this vein, Martinez et al. [53], who evaluated the CaL retrofit to both sub-critical and supercritical CFPPs, indicated that the efficiency penalties would be smaller for CaL retrofitted to supercritical CFPPs.

The studies reviewed previously assumed that the calciner is fuelled with the same fuel as the reference CFPP. A study by Hanak et al. [31]

evaluated the effect of fuel used in the calciner on the efficiency penalty of the CaL retrofit to a 580 MW_{el} supercritical CFPP. This study revealed that partial (20%) and complete substitution of coal with biomass in the calciner can lead to reduction in the efficiency penalty from 7.9% points to 7.7% and 7.4% points, respectively. This is primarily a result of lower CO₂ capture level in the calciner, as biomass can be considered as a CO₂-neutral fuel, and less ash being circulated in the system; hence less heat required for solids preheating in the calciner. A large reduction in the efficiency penalty to 6.7% points was also observed for the case of a natural gas-fired calciner, which was primarily due to no ash accumulation in the system. It must be stressed that the reviewed studies indicated that the CaL retrofits would result in lower efficiency penalty compared to chemical solvent scrubbing, which was shown to result in efficiency penalty of 9% points (chilled ammonia scrubbing) [54] and 9.5% points (monoethanolamine scrubbing) [31] when retrofitted to the same CFPP. Nevertheless, all of the reviewed studies assessing the CaL retrofitted to the CFPP concluded that the main sources of the parasitic load result from the power requirement of the ASU and the CCU. For this reason, the main reduction in the efficiency penalty associated with CaL can be primarily achieved via reduction of the heat requirement in the calciner, utilising alternative options to provide heat for sorbent regeneration and thus avoiding the need for oxygen production in the energy-intensive ASU.

A wide range of measures for reduction of the efficiency penalty associated with CaL retrofits to CFPPs has been reported in the literature. These measures focus primarily on improving the heat integration within both the CaL process itself, and between CaL and CFPP. This aims at reducing the heat requirement in the calciner and increasing the degree of heat utilisation in the entire system. Such an improvement can be realised via application of a systematic heat exchanger network (HEN) analysis, which is regarded as an industrial standard to maximise the heat utilisation within the system. Lara et al. [55,56] have employed such an approach to maximise the techno-economic performance of the CaL retrofit to a 500 MW_{el} supercritical CFPP, which was characterised with the net efficiency of 38.2%. Their studies have shown that the efficiency penalty can be reduced from 6.4% points to between 5.2% points [55] and 6.2% points [56] on an improvement in the heat integration of the entire system. Moreover, a study by Vorrias et al. [57], which evaluated the retrofit of CaL to a 330 MW_{el} supercritical CFPP using lignite as a fuel, has indicated that heat integration has the potential to significantly reduce the efficiency penalty. Primarily, deployment of a solid-solid heat exchanger (Fig. 2a), which

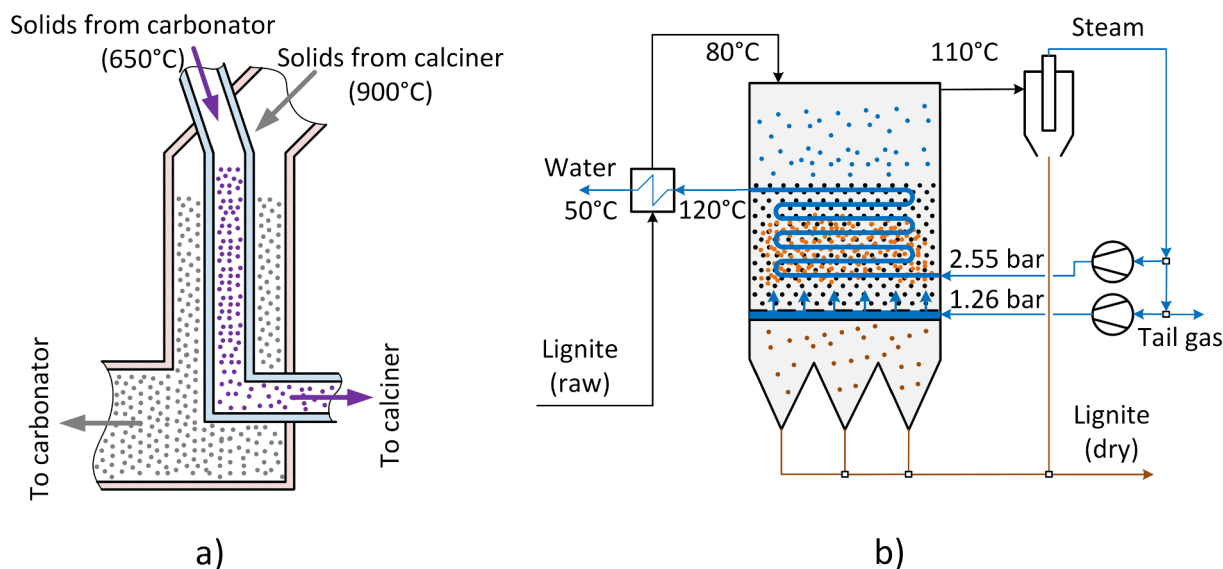


Fig. 2. Representation of (a) solid-solid heat exchanger and (b) lignite bubbling fluidised bed dryer (Adapted with permission from Vorrias et al. [57]. Copyright 2013 Elsevier.).

allows preheating the solids entering the calciner against the solids leaving the calciner, was shown to reduce the heat requirement from fuel oxy-combustion in the calciner. As a result, the efficiency penalty associated with such a system was found to be 5.1% points. Further improvement of 0.1% point was achieved via implementation of a lignite dryer (Fig. 2b) that utilised recompressed steam as a fluidising medium and was designed to reduce the moisture content in lignite to a level comparable to that of hard coal [58]. Again, the efficiency penalty estimated for the CaL retrofit was shown to be 2.9% points lower compared to that of a corresponding CO₂ capture plant using chemical solvents (monoethanolamine) and 0.9% points lower than that of an oxy-fuel CFPP using lignite as a fuel. This has further proved the thermodynamic benefits of CaL retrofits to CFPPs compared to other CO₂ capture technologies. In this vein, a study by Ortiz et al. [59] has shown that the efficiency penalty associated with the retrofit of CaL to a 561 MW_{el} subcritical CFPP, which is characterised with a net efficiency of 33.5%, can be improved by 0.2% points on implementation of a solid-solid heat exchanger. Such an improvement arose primarily from both a reduction in the fuel and oxygen requirements in the calciner, which can be lower by up to 16.5%, and a 2% point increase in the thermal efficiency of CaL according to a study by Martinez et al. [60]. However, technically and economically feasible devices for heat transfer between two solid phases must first be developed.

Alternative concepts that utilise existing and industrially proven equipment were proposed by Martínez et al. [60,61]. The first concept included a single mixing seal valve for both the carbonator and the calciner that allows direct heat transfer between the solids leaving these reactors [60]. This configuration was deemed as bringing no thermodynamic improvement over the conventional CaL process, primarily due to reduced fraction of active CaO entering the carbonator. The second concept included an additional heat recovery fluidised bed, in which the sensible heat of the CO₂ stream leaving the calciner is recovered to preheat the solid particles from the carbonator [60]. Although the concentrated CO₂ stream mixed with the partially carbonated solid particles from the carbonator, no carbonation reaction could occur. This is because the fast carbonation reaction cannot proceed, as

the active CaO is trapped in the core of each solid particle, the surface of which has been covered with the calcium carbonate (CaCO₃) layer formed in the carbonator [62]. Despite the fact that the heat requirement in the calciner was still satisfied via direct oxy-fuel combustion, the fuel and oxygen requirements would be reduced by up to 9.7%, and the thermal efficiency of CaL can be improved by 1.4% points. The third concept utilised cyclonic preheaters, which are used in the cement industry, in place of the heat recovery fluidised bed (Fig. 3) [61]. In this additional piece of equipment, heat available in the CO₂ stream leaving the calciner was utilised to preheat solids leaving the carbonator to around 725 °C prior to entering the calciner. Although implementation of the cyclonic preheater has not changed the net efficiency of the retrofitted system, it reduced the energy requirement of the calciner. This was shown in reduction of the coal and oxygen requirements by up to 13.3%, with respect to the conventional CaL process.

Regardless of the potential for a significant reduction in the heat requirement, and thus fuel and oxygen requirements in the calciner, the concepts reviewed above still require the energy-intensive and expensive cryogenic ASU for direct oxy-fuel combustion in the calciner. Interestingly, this requirement can be completely alleviated by indirect heat transfer from another heat source. Abanades et al. [42] proposed an alternative design of the calciner in which the heat for sorbent regeneration is supplied through the metallic walls from a fluidised bed combustor fueled with an air and fuel mixture that operates at 1050 °C. In such a design, the calciner can be operated at 850 °C, which is lower than the temperature of 875–950 °C considered in the previous studies, as steam was used as the fluidising medium. Yet, although this configuration would be characterised by higher thermal efficiency and no requirement for oxygen production, it would require materials that have not yet been tested in practice. Also, close integration of the combustor and the calciner is required, as a considerable heat transfer area of 800 m² is required. Despite the engineering challenges, this configuration was reported to impose an efficiency penalty of 6.6% points, which is 1.6% points less than for the conventional CaL configuration. More recently, the use of heat pipes as a mean for indirect heat transfer between the calciner and the combustor, which operated

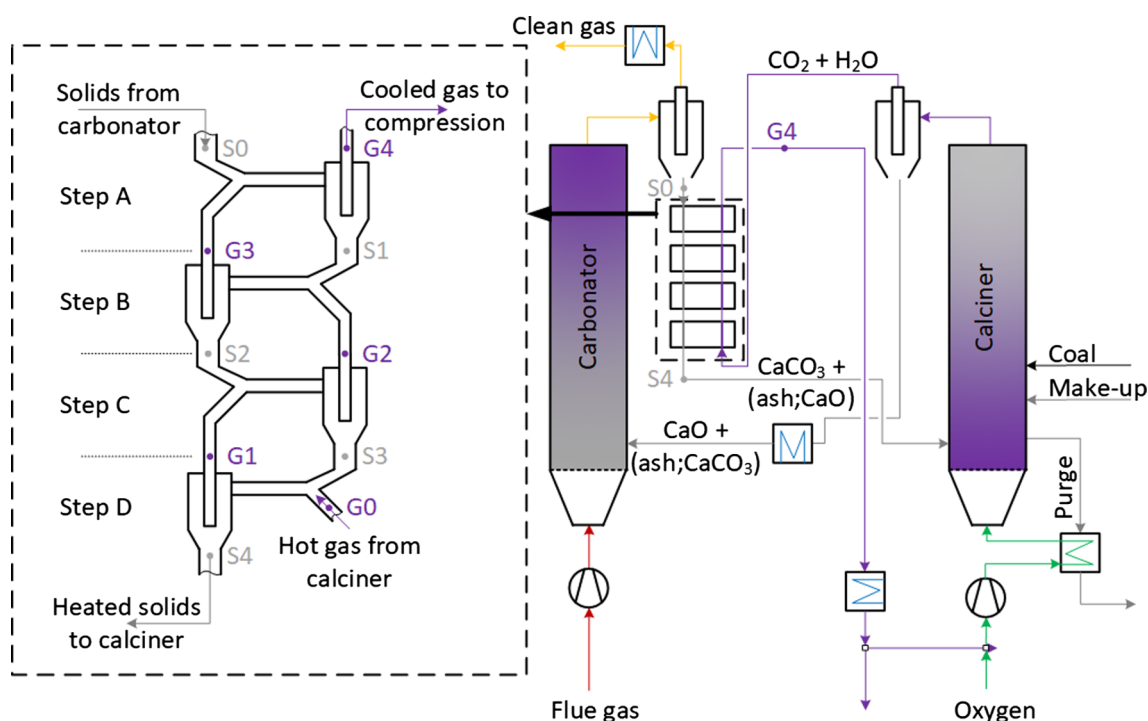


Fig. 3. Improvement of carbonate looping process performance through implementation of the cyclonic preheater (Adapted with permission from Martínez et al. [61]. Copyright 2013 American Chemical Society.).

at 1100 °C, have been experimentally proven [44]. The retrofit of such an indirectly-heated CaL to the 1100 MW_{el} supercritical CFPP was shown to result in an efficiency penalty of 1.8–2.3% points (without compression), depending on the sorbent conversion in the carbonator. This was found to be 1% point lower than the corresponding retrofit of the conventional CaL process to the same reference CFPP [45]. To avoid using untested materials, an alternative to reduce the heat requirement in the calciner is the concept of calcination driven by heat carriers that was first proposed by Abanades et al. [42]. Similarly to the concept of the indirectly-heated calciner, this process includes an additional circulating fluidised bed combustor in which fuel is burned in an excess amount of air. The bed material, which is a dense solid material such as aluminium oxide (Al₂O₃) or deteriorated sorbent, is heated up directly in the combustor, separated from the flue gas stream, and then fed to the calciner to provide heat for sorbent regeneration. However, it is still not clear whether continuous separation of the sorbent and the heat carrier based on the difference in their densities would be possible at the required scale. Nevertheless, the net efficiency of the retrofit scenario based on such a system is claimed to be 2.2% points higher than that of the conventional CaL retrofit [42]. Finally, the heat for sorbent regeneration in the calciner can be driven by the heat from a chemical looping system [40], which uses oxygen carriers to transfer oxygen from air to the fuel. The combined calcium and chemical looping system includes an additional reactor – air reactor – in which the oxygen carrier reacts with oxygen in air. The oxidised oxygen carrier is then reduced by the gaseous fuel in a fuel reactor, providing heat for calcination (Fig. 4). This system was considered to operate as either a single- or dual-loop process [38], depending on whether the oxygen carrier is mixed with the sorbent and reduced directly in the calciner, or is handled separately in another loop. In the latter case, the heat is transferred to the calciner indirectly. The efficiency penalty associated with the combined calcium and chemical looping process was estimated to be between 3.6 and 6.9% points [39] and 5.2–6.3% points [38] for the single- and dual-loop process, respectively. Although the efficiency penalty of such a process was found to be 2.5–3% points lower than that of CaL retrofitted to the same reference CFPP, the required solids looping rate to achieve the same CO₂ capture level was at least one order of magnitude higher than that in CaL [38]. This imposes an additional efficiency penalty associated with the requirement for handling more solids. Yet, such a high circulation rate was required due to the low oxygen carrier-to-sorbent ratio in the considered system. Therefore, the concept needs to be further explored considering higher content of oxygen carrier in the solid material required to meet the heat requirement for sorbent regeneration.

It must be stressed that all reviewed studies considering CaL retrofitted to CFPPs assumed that the high-grade heat is utilised to raise high-pressure steam for the secondary steam cycle. Yet, the study by Hanak et al. [63] has highlighted that CaL operates within a similar temperature range to the bottoming cycle of NGCC (600 °C), nuclear reactors (500–1000 °C), and concentrating solar power plants (500–1000 °C). Therefore, it proposed to use advanced power cycles, such as a supercritical CO₂ cycle, for utilisation of the high-grade heat from CaL. The analysis of CaL retrofitted to a 580 MW_{el} supercritical CFPP indicated that by using the supercritical CO₂ cycle in place of the supercritical steam cycle, the efficiency penalty can be reduced by 1% point, if the turbine inlet conditions are the same. On increase of the turbine inlet pressure from 242 bar to 300 bar and temperature from 593 °C to 620 °C, the efficiency penalty was further reduced by 0.6% point, to 6.3% points. Further improvement in the thermodynamic performance can be obtained via implementing an additional inter-cooling stage and replacing the first main compressor with a pump that can bring the efficiency penalty down to 5.8% points. This was shown to be 2.1% points improvement over the conventional CaL process. Therefore, consideration of advanced power cycles, such as the supercritical Brayton cycle, for utilisation of high-grade heat from CaL, has the potential for considerable reduction in the efficiency penalty

associated with this technology, especially when linked with the alternative concepts reviewed above.

The main engineering challenge of CaL, which needs to be addressed prior to commercial deployment of this technology, is degradation of the sorbent performance after a number of calcination and carbonation cycles. This can be associated primarily to sintering, attrition and sulphation of the sorbent, leading to the requirement for sorbent make-up [18]. Conversion of the sorbent can be improved via doping, thermal pre-treatment, chemical treatment, and reactivation [22].

Hydration has been proven via thermogravimetric analysis [64] and pilot-scale tests [65] as one of the most viable options to improve sorbent performance. Its benefits on the thermodynamics of the CaL retrofit to CFPPs was investigated by Wang et al. [34,35] and Hanak et al. [66]. In such a process, the sorbent is reactivated on contact with steam in the hydrator (Fig. 5). Wang et al. [34] have analysed integration of this concept into a 561 MW_{el} subcritical CFPP and high-grade heat from the CaL process was used to generate high-quality steam that is sent to the primary cycle, replacing part of the steam generated in the power boiler. This means that the existing boiler would need to operate in the part-load mode. The thermodynamic performance assessment indicated that a maximum net efficiency of 26.9% could be reached if the calciner was indirectly heated using the flue gas from the combustion process. On the other hand, when the calciner was directly heated through oxy-fuel combustion of coal or natural gas, the net efficiency decreased to 26.5% and 26.1%, respectively. Such values for net efficiency are considerably lower than those reported previously. The main reason behind this is the low net efficiency of the reference CFPP. Nevertheless, the maximum efficiency penalty was estimated to be 7.4% points, which is in line with the figures reported in other studies. Furthermore, Wang et al. [35] have shown that the efficiency penalty for the CaL process with sorbent reactivation via hydration is 22.2% lower than that for the conventional CaL process. Conversely, Hanak et al. [66] have shown that implementing the hydration concept to reactivate the sorbent would only reduce the efficiency penalty by 0.3% points, from 8.7% points to 8.4% points. As the latter process operates on higher average conversions, this reduction can be associated with reduction of the solid looping rates between the reactors, which leads to a decrease in the heat requirement in the calciner. Nevertheless, a lower improvement in the net efficiency on implementing hydration in the study by Hanak et al. [66] could be

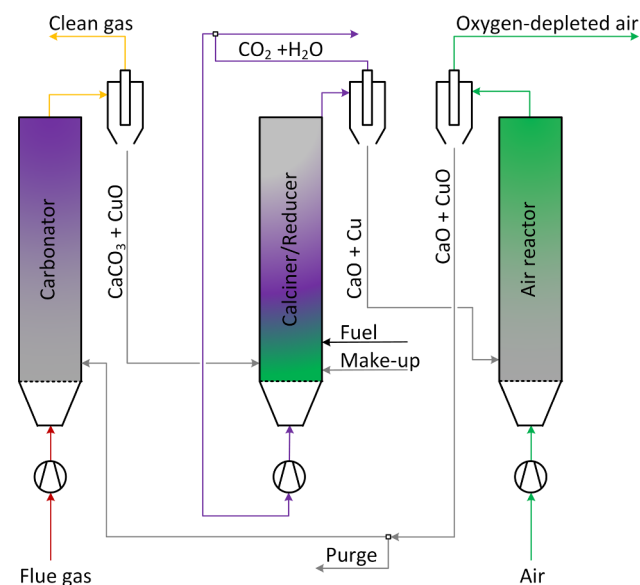


Fig. 4. Combined calcium and chemical looping single-loop process (Adapted with permission from Duhoux et al. [38]. Copyright 2016 Wiley.).

the CaL retrofit, an increase in the sorbent reactivity would reduce the amount of the sorbent required to achieve the same CO₂ capture level, and thus could result in an improvement of the economic performance. As a result, the cost of CO₂ avoided can be lower for dolomite (18.6 €/tCO₂) compared to limestone (15.8–19 €/tCO₂), under particular operating conditions. This was mostly because of the comparable prices of limestone and dolomite of 6–10 €/t. Importantly, although alumina-doped limestone and lithium orthosilicate (Li₄SiO₄) were shown to experience considerably lower degradation than natural sorbents, their high price of 240–310 €/t and 27,000 €/t, respectively, resulted in the cost of CO₂ avoided to be higher (22–300 €/tCO₂) than that of limestone and dolomite. Therefore, a substantial drop in the material cost is required for these sorbents to be used at commercial scale to ensure that the CaL retrofit is feasible from both technical and economic standpoints. Furthermore, Hanak et al. [66] showed that the techno-economic feasibility of the CaL retrofit to a CFPP would be improved upon implementation of the sorbent reactivation via hydration. This study not only indicated that such solution would result in a reduced efficiency penalty, but also in an 18% reduction in the cost of CO₂ capture and a 6% reduction in the specific capital cost. In addition, studies by Abanades et al. [70], Cormos [72], and Cormos and Cormos [73] proved that the LCOE can be reduced by increasing the steam conditions in the conventional steam cycles, hence their net thermal efficiency. Interestingly, in the latter studies [72,73], the cost of CO₂ avoided was found to increase with the steam conditions in the conventional steam cycle. This, however, can be associated to the capture rate (higher by 3.3%) in the case when CaL is retrofitted to a supercritical CFPP. Finally, the deterministic studies reviewed indicated that the cost of CO₂ avoided has the potential to be lower (7–87.5 €/tCO₂) [47,66,70–74] compared to that of mature chemical solvent scrubbing (35–75 €/tCO₂) [73,75–78], proving the potential for economic feasibility of CaL retrofits to CFPPs.

3.2. Natural gas combined cycle power plants

Berstad et al. [46,79] were the first to analyse the feasibility of retrofitting CaL downstream of the gas turbine in a 416.4 MW_{el} NGCC (Fig. 6), that was characterised with a net efficiency of 58.4%, under a range of operating conditions for the secondary steam cycle, heat integration configurations, and sorbents. The benchmark configuration that assumed the recovery of high-grade heat from CaL in the sub-critical secondary steam cycle, was shown to result in an efficiency penalty of 12.0% points. Such performance was considerably worse compared to the same NGCC retrofitted with chemical solvent scrubbing using monoethanolamine, which resulted in an efficiency penalty of 8.6% points, and indicated that a CaL plant may not be a preferable option for NGCCs. This can be attributed primarily to the low CO₂ concentration in the flue gas. The net efficiency of the CaL retrofit was found to improve by 1.7% points upon changing the operating conditions of the secondary steam cycle from sub- to super-critical, which was a result of the higher efficiency of the high-grade heat utilisation. This implies that there is the potential for further reduction in the efficiency penalty by implementing more efficient power cycles, such as the supercritical CO₂ cycle [63]. Further improvement in the net efficiency of 0.8% points was obtained on implementing the solid-solid heat recuperator, reducing the efficiency penalty to 10.0% points [79]. This was a result of reducing the temperature difference between the reactors, and thus reducing the fuel and oxygen requirements to sustain the desired calciner temperature. Importantly, oxy-combustion of natural gas in the calciner will result in a significant fraction of moisture in the gas phase inside this reactor (30–40%_{vol}). Therefore, the calciner can be efficiently operated at lower temperature [46], leading to further reduction in the temperature difference between the reactors. This modification, along with implementing hot CO₂ recycle and optimising the fresh sorbent make-up ratio, resulted in 2.9% points improvement in the net thermal efficiency, reducing the efficiency penalty to 7.1% points [46].

Such improvement in the thermodynamic performance of the CaL retrofit makes it clear that this technology can compete with more mature chemical solvent scrubbing systems.

Similarly to the study by Berstad et al. [79], Hu and Ahn [80] indicated that the retrofit of CaL to NGCC, which comprised an F-class gas turbine and sub-critical primary steam cycle, was less favourable compared to chemical solvent scrubbing using monoethanolamine. However, they proposed implementing exhaust gas recirculation to increase the CO₂ concentration in the flue gas entering the carbonator from ~4%_{vol} to ~7%_{vol}. Such configuration was found to reduce the efficiency penalty associated with the CaL retrofit from 10% points to 8.6% points. Regardless of such an improvement, the net efficiency of the CaL retrofit was still 0.9% point lower than the corresponding chemical solvent scrubbing retrofit with exhaust gas recirculation. However, if the improvement measures proposed by Berstad et al. [46,79] were implemented, a substantial reduction in the efficiency penalty below 7% points could be achieved. Yet, application of these configurations must be economically substantiated. This is because implementation of exhaust gas recirculation and supplementary firing in a chemical solvent scrubbing retrofit to a NGCC was shown to increase the capital cost by 20%, while reducing the LCOE by only 6% [81].

As indicated above, the main challenge of CaL using natural sorbents, such as limestone (calcite), is rapid degradation of sorbent performance over a number of cycles. Importantly, an increase in the average carbonation conversion from 18.6% (calcite) to 24.8% (dolomite) and 34.2% (synthetic CaO), resulted in an efficiency penalty reduction of 0.2% and 0.8% points, respectively [46]. Yet, such increase in the thermodynamic performance should be substantiated by benefits in the economic performance. This is particularly important in the case of the synthetic sorbents that are characterised by much higher specific costs [68].

Unfortunately, information on the economic feasibility of CaL retrofits to NGCCs in the current literature is limited to a few studies by Cormos and Cormos [82,83], and Erans et al. [84]. The former studies assessed the techno-economic performance of CaL retrofitted to a 498 MW_{el} NGCC comprised of an M701G2 (Mitsubishi Hitachi Power Systems) gas turbine and a subcritical primary steam cycle, with a net efficiency of 58.6%. The thermodynamic performance of the system reduced by 9.4% points on the CaL retrofit, higher than the efficiency penalty of 5.9% points reported for chemical solvent scrubbing using methyl diethanolamine. Although this is in line with the estimations made by Berstad et al. [79] and Hu and Ahn [80], Cormos and Cormos [82,83] reported that the LCOE of 56.9 €/MWh for the CaL retrofit was 16.2% lower compared to the chemical solvent scrubbing retrofit. Moreover, the cost of CO₂ avoided for the CaL retrofit (33.8 €/tCO₂) was estimated to be nearly half that for the chemical solvent scrubbing retrofit (67.1 €/tCO₂), and the specific capital cost was 30.2% lower. Similar results were presented by Erans et al. [84], who evaluated the techno-economic performance of CaL retrofitted to an 820 MW_{el} NGCC that was characterised with the net efficiency of 57.7%. This study also compared the effect of the location of CaL with respect to the primary steam cycle on the net efficiency of the system. Importantly, retrofitting the CaL downstream of the primary steam cycle resulted in a much higher efficiency penalty (12.0% points) compared to the upstream location (8.6% points). This resulted from the high volume of flue gas that needed to be preheated prior to entering the carbonator to maintain the desired operating temperature. Hence, the amount of high-grade heat available for recovery in the secondary steam cycle was lower, reducing the net efficiency of the entire system. Nevertheless, the retrofit of CaL upstream of the primary steam cycle was shown to result in a cost of CO₂ avoided of 29.3 €/tCO₂, which is comparable to the figure reported by Cormos and Cormos [82,83]. Importantly, in these studies [82–84], the LCOE increased by 25.6–33.2% with respect to that estimated for the reference NGCC without CO₂ capture.

4. Greenfield power generation systems

As has been shown above, CaL can be seen as the technically and economically feasible option to decarbonise the existing fleet of fossil fuel-fired power generation systems, especially when novel process configurations, improved sorbent performance via hydration, high degree of heat integration, and utilisation of advanced power cycles for high-grade heat recovery are considered. The main feature of CaL, however, is its high-temperature operation that creates an opportunity for this technology to act as a power boiler in novel power generation systems. This enables further reductions in the economic and efficiency penalties, as well as supports wide deployment of low-carbon power generation technologies. Therefore, similarly to the measures aimed to reduce the efficiency penalty associated with CaL retrofits to fossil fuel-fired power generation systems, a number of alternative process configurations for novel CFPPs were developed that were characterised with much lower CO₂ emissions compared to those of conventional systems (Section 4.1). Moreover, the need for high-efficiency and low-emission fossil-fuel power generation systems has led to the development of novel integrated gasification combined cycle (IGCC) power plants that have the potential to improve both thermodynamic and economic performance compared to the conventional CFPPs (Section 4.2).

Substitution of fossil fuels with biomass [4] or cost-effective production of clean fuels, such as hydrogen, is predicted to contribute towards decarbonisation of the power sector. A combination of CCS with hydrogen production is considered to be the least cost-intensive option among other hydrogen production technologies [85]. A number of sorption-enhanced steam reforming (SESR) concepts based on CaL, especially using Ca-based sorbent, have been recently developed (Section 4.3). These have been shown to significantly enhance the quality and economics of hydrogen production from reforming of liquid and gaseous fuels with simultaneous CO₂ capture [86–91]. Importantly, with NGCC being a well-established commercial technology with high efficiency and reliability, and low capital costs [90], the novel low-carbon concepts based on that technology can be expected to be characterised by more favourable techno-economic performance compared to novel CFPPs [92,93] and could become commercially available in a relatively short timeline. Yet, for such concepts to use hydrogen-rich fuel instead of natural gas, conventional gas turbines need to be adapted, mainly by reducing the operating temperatures and partially closing the compressor variable guide vanes, to consider changes in the volumetric flow rate and the thermophysical properties of hydrogen-rich fuels [94].

4.1. Combustion-based coal-fired power plants

Building on the concept proposed by Abanades et al. [42] in which the calcination process was driven by heat carriers, Martinez et al. [41] proposed a novel CFPP using a three-fluidised-bed combustion system based on CaL (Fig. 7). In this process, the heat required to calcine the sorbent was provided by heating both a part of the calcined sorbent from the calciner and fuel ash up to 1030 °C. These solids were heated in the air-fired circulating fluidised bed combustor, indicating that there was no need for energy-intensive ASU. Importantly, flue gas from the combustor was directly fed to the carbonator and, thus, the proposed process can be seen as a standalone CFPP with two heat sources (combustor and carbonator) and a single heat sink (calciner). Having integrated these heat sources, along with several hot solid and gas streams, with the supercritical steam cycle, Martinez et al. [41] have shown that the net efficiency of such a process can reach 37.8%, considering the power requirement of the CCU. This was shown to be 4.3% points higher than a comparable oxy-fired CFPP, proving the thermodynamic feasibility of this novel concept. However, it needs to be pointed out that the calcined sorbent would be exposed to temperatures higher than 1000 °C upon heating in the combustor, which may cause

enhanced sintering and deactivation [95]. Therefore, evaluation of the effect of increased sorbent deactivation on the techno-economic performance of the three-fluidised-bed combustion system based on CaL should be conducted to prove its feasibility under such operating conditions.

Strelow et al. [96] proposed integrating a pressurised calciner, which is an entrained flow reactor, inside a coal-fired combustor (Fig. 8). To enable efficient operation of the calciner under higher pressure (2–3 bar) and 900 °C, superheated steam was injected into that reactor. Importantly, in addition to utilising the high-grade heat to raise steam for the supercritical steam cycle, which is a generally used practice in the state-of-the-art CaL concepts [7], the CO₂-H₂O stream leaving the calciner at a higher pressure was used in the steam turbine to generate an additional amount of power. The assessment of the thermodynamic performance of this concept was shown to impose an efficiency penalty 4.4% points, considering the power requirement for the CCU. This further proves that indirect heat transfer can not only substantially reduce the energy intensity of the ASU, but also lead to development of novel CFPPs. Therefore, development of the indirectly-heated calciner technology has the potential to provide a substantial reduction in the energy intensity of CaL, and bring this technology closer to commercialisation [42].

In this vein, Hanak and Manovic [36] have recently proposed a calcium looping combustion (CaLC) process for high-efficiency, low-emission power generation (Fig. 9). In this process, the heat for sorbent calcination is provided indirectly from an external coal-fired combustor and the resulting flue gas is directed to the carbonator for CO₂ capture. Considering the CaLC as a power boiler, similarly to the approach applied by Martinez et al. [41], to raise high-pressure steam for the supercritical steam cycle, the net efficiency of the entire system was estimated to be between 33.7% and 35.6, which was 2.4–4.3% points lower than the reference CFPP operating under the same steam conditions. This was mainly associated with the power requirement of the CCU and the amount of high-grade heat available for power generation in the supercritical steam cycle under different operating conditions. Importantly, a reduction in the efficiency penalty in this concept compared to the concepts proposed by Martinez et al. [41] and Strelow et al. [96] can be attributed to a higher degree of heat integration in CaLC, as in this concept the heat integration between solid and gas streams, and optimisation of the fresh limestone make-up stream were considered. Such improvements are consistent with the results presented by Lara et al. [55,97] who utilised a systematic heat exchanger

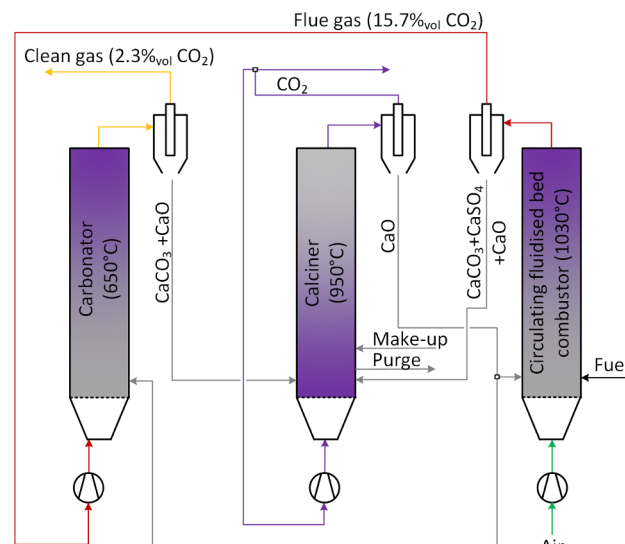


Fig. 7. Concept of the three-fluidised-bed combustion system based on carbonate looping (Adapted with permission from Martínez et al. [41]. Copyright 2011 Elsevier.).

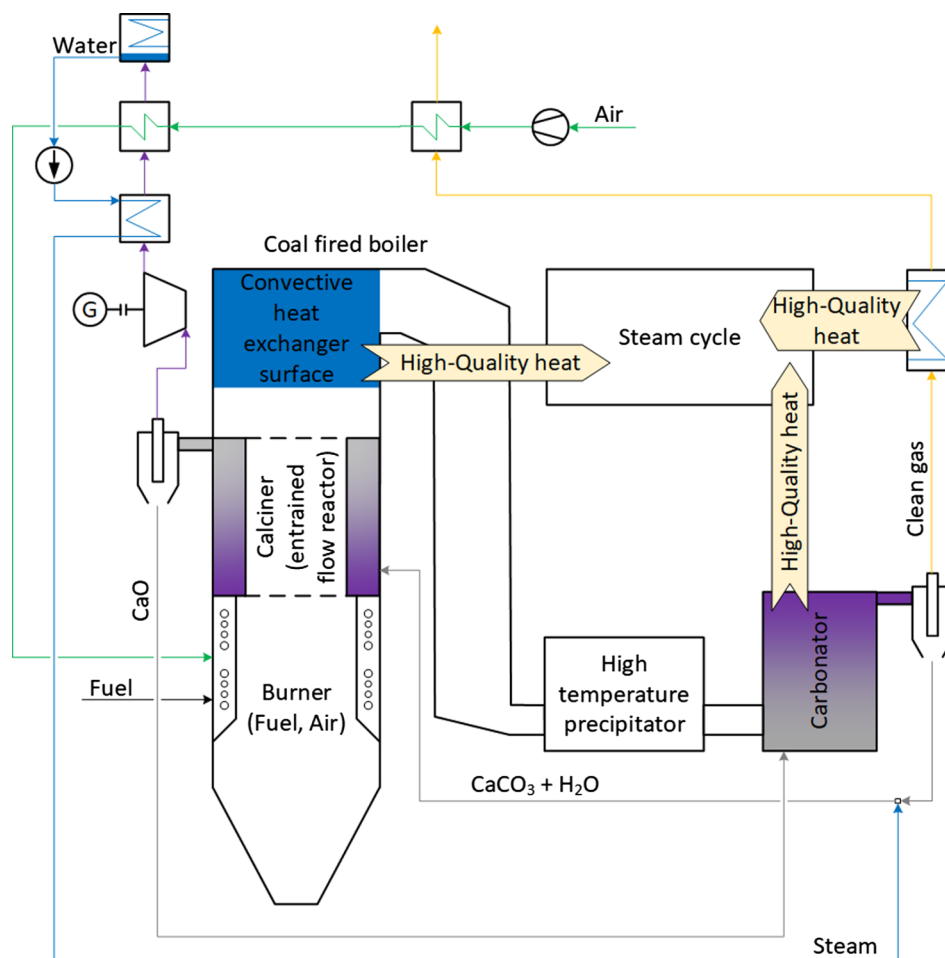


Fig. 8. Concept of pressurised carbonate looping integrated with coal-fired combustor (Adapted with permission from Strelow et al. [96]. Copyright 2012 Wiley.).

network analysis to improve the heat integration in CaL retrofitted to a CFPP. Importantly, the cost of CO₂ avoided associated with CaLC was shown to vary between 30 €/tCO₂ and 40 €/tCO₂, which is comparable to the lower end of the range reported for the CaL retrofit scenarios that can reach figures as high as 87.5 €/tCO₂ [69,71].

In addition to exploring alternative options for providing heat to the calcination process, application of hybrid CO₂ capture processes, which combine two or more CO₂ capture technologies, has been considered as a potential option to overcome the drawbacks of standalone technologies [98]. Romano [99] proposed a hybrid system that used CaL to remove CO₂ from the CO₂ purification and compression unit (CPU) vent gas stream in a 719 MW_{el} oxy-fuel ultra-supercritical CFPP (Fig. 10). The thermodynamic evaluation of such a process indicated that implementation of CaL resulted in an increase in the efficiency penalty of 0.8% points, compared to that for the standalone oxy-fuel ultra-supercritical CFPP (6.9% points). This was mostly associated with the heat requirement for limestone calcination and lime export, as well as slightly higher CPU power requirement. Importantly, a slight improvement of 0.4% point was achieved via sorbent re-carbonation in the boiler. Regardless of the negative effect on thermodynamic performance, the main benefit of such a hybrid process was a high CO₂ capture level of more than 99%. Hence, it can be expected that despite a higher efficiency penalty, such a hybrid process can achieve better economic performance when the carbon tax is higher.

Another hybrid process that links oxy-fuel combustion CFPP with CaL has been proposed by Ortiz et al. [100]. In this process, the fuel is partially oxy-combusted in a CFPP to increase the concentration of CO₂ in the flue gas to 30–60% vol, as opposed to 15% vol in a conventional air-combustion CFPP. This aims to increase the driving force for the

carbonation reaction, thus enhancing the CO₂ capture of the sorbent. An assessment of the thermodynamic performance of such a hybrid process showed that the efficiency penalty varied between 8.7% points to 9.2% points. As this was found to be close to the figures estimated for conventional CaL (7.5% points) and oxy-fuel combustion CFPP (9.1%), implementation of such a hybrid process was found not to contribute towards reduction of the energy intensity of CaL. Nevertheless, the main benefit of linking CaL with partial oxy-fuel combustion was the potential for reduction of the solids inventory and fresh sorbent make-up rate needed to achieve the same CO₂ capture level compared to conventional CaL. This implied that the size of the CaL unit can be reduced, which could lead to reduction of the economic penalty associated with CO₂ capture. However, similarly to the process proposed by Romano [99], economic assessment needs to be undertaken to assess the economic feasibility of such hybrid processes.

4.2. Integrated gasification combined cycle power plants

The feasibility of integration of the IGCC with CaL as the post-combustion CO₂ capture plant was first evaluated by Li et al. [101]. In such a process (Fig. 11), coal was partially oxidised with a mixture of steam and air in a fluidised bed gasifier to form syngas and char. The former product was cleaned in acid gas (SO₂, H₂S) and fly ash removal systems, and then utilised in the gas turbine and the resulting flue gas was sent to the carbonator for CO₂ capture. The latter product was oxy-combusted in the calciner to provide heat for sorbent regeneration. In addition, the high-grade heat from CaL was utilised in the sub-critical steam cycle for additional power generation. The thermodynamic feasibility assessment has indicated that if limestone is used as a sorbent

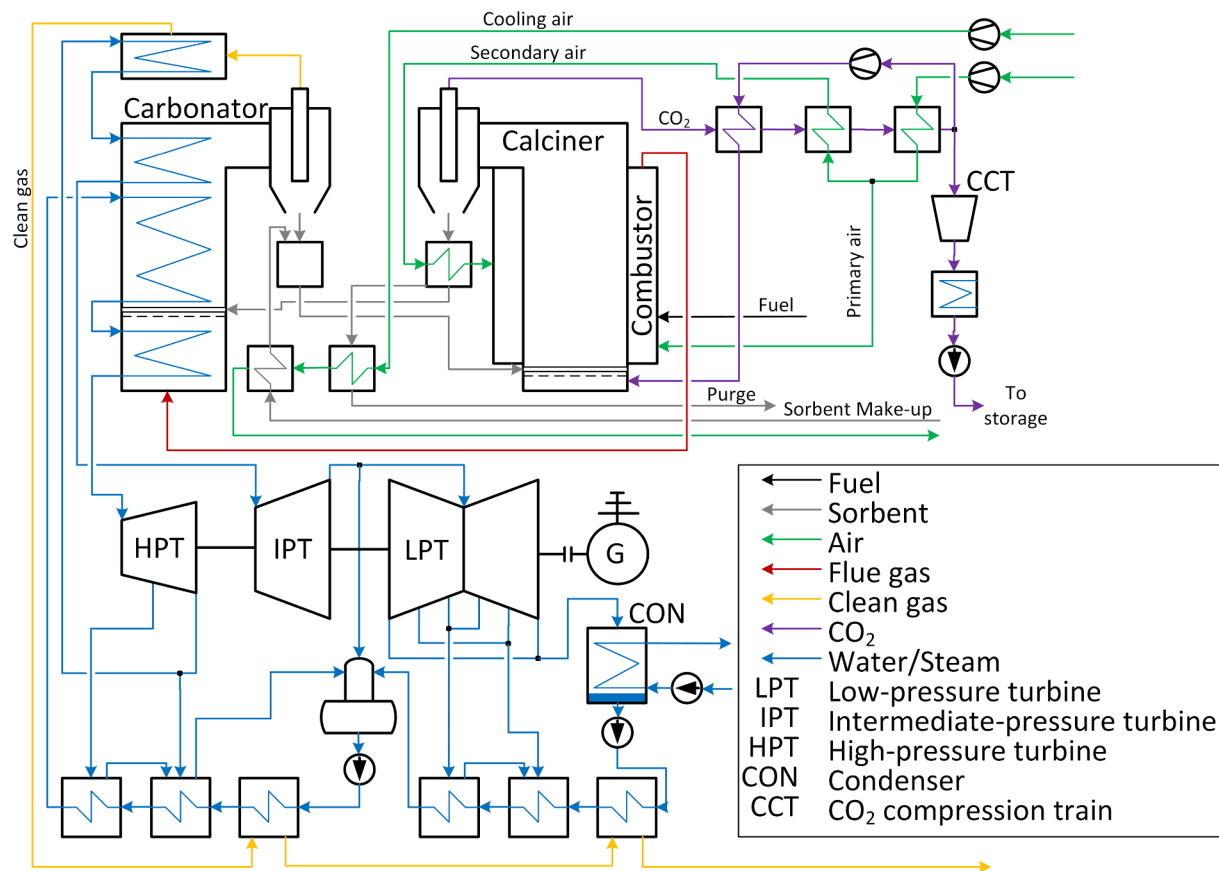
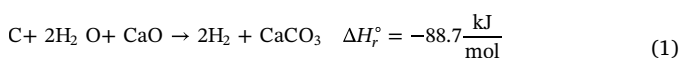


Fig. 9. Calcium looping combustion for high-efficiency low-emission power generation (Adapted with permission from Hanak and Manovic [36]. Copyright 2017 Elsevier.).

and depending on the amount of sulphur in the char, such a process can achieve a net efficiency of 41.0–41.7%. Importantly, if Ca-based sorbent modified with acetic acid was utilised, the net efficiency can reach 42.4–43.1%, while removing 90% of CO₂. Such a figure is higher compared to the range of 28.6–40.2% reported for novel combustion-based CFPPs (Section 4.1). Yet, the feasibility of using such modified sorbent needs to be substantiated from both technical and economic standpoints.

The concept evaluated by Li et al. [101] followed the state-of-the-art concepts for decarbonisation of the conventional CFPPs that were retrofitted with CaL as the post-combustion system. However, in IGCC power plants, CO₂ capture can be implemented as either a post-combustion system for CO₂ capture from flue gas, or a pre-combustion system for CO₂ capture from syngas. Therefore, it can be expected that using CaL as the pre-combustion CO₂ capture plant in an IGCC would reduce the energy requirement for sorbent regeneration due to a higher partial pressure of CO₂ in syngas compared to flue gas. Moreover, CaL has been shown to enhance the water-gas shift reaction, yielding a high-purity hydrogen stream, and thus increasing the quality of syngas [102]. This is because, in the sorption-enhanced gasification process, the net reaction of which is shown in Eq. (1), CaO will remove CO₂ produced in the water-gas shift reaction, shifting the equilibrium to the right and promoting high-purity hydrogen production [103].



The techno-economic feasibility of these concepts were compared by Cormos and Cormos [102,104], who used a 561 MW_{el} IGCC power plant characterised with a net efficiency of 44.4% as a reference. The thermodynamic assessment indicated that the net efficiency of the entire system reduced by 10.1% points and 7.3% points for the post-

combustion and pre-combustion configuration, respectively. This implied that the performance of the IGCC with CaL for the post-combustion CO₂ capture was comparable with that associated with conventional post-combustion scrubbing technologies. Hence, similarly to retrofits of conventional CaL to NGCC evaluated by Berstad et al. [46,79] and Erans et al. [84], such application of this technology will not bring any benefits in terms of process thermodynamic performance. Conversely, the pre-combustion configuration was found to result in an efficiency penalty 1–2% points lower than conventional pre-combustion solvent scrubbing technologies. Furthermore, the economic assessment has confirmed the superiority of the pre-combustion configuration, as the associated LCOE and cost of CO₂ avoided for this configuration were 76.1 €/MW_{el}h and 26.3 €/tCO₂, compared to 78.1 €/MW_{el}h and 29.2 €/tCO₂ for the post-combustion configuration, respectively [84]. It needs to be pointed out that the economic performance, including the specific capital cost, is comparable to that of the CaLC concept proposed by Hanak and Manovic [36]. Therefore, the pre-combustion configuration has been deemed as a more suitable for IGCC power plants and has been further evaluated.

A study by Wang et al. [105] analysed an IGCC power plant fueled with high-purity hydrogen produced via sorption-enhanced gasification of coal in a dual-fluidised-bed system (Fig. 12). In such a system, the gasifier reactor was divided in two sections, a gasification section, in which allothermal steam gasification of coal took place, and a carbonation section, where carbon monoxide (CO) was shifted to CO₂ that was then removed on contact with CaO. It has been assumed that only part of the coal was converted in the gasifier reactor (45–60%) and the unreacted char was fed to the calciner. Oxy-combustion of that amount of fuel was shown to be sufficient for sorbent regeneration in the calciner. The high-purity hydrogen stream was then utilised in an F-class gas turbine and the high-grade heat was converted into electricity in a

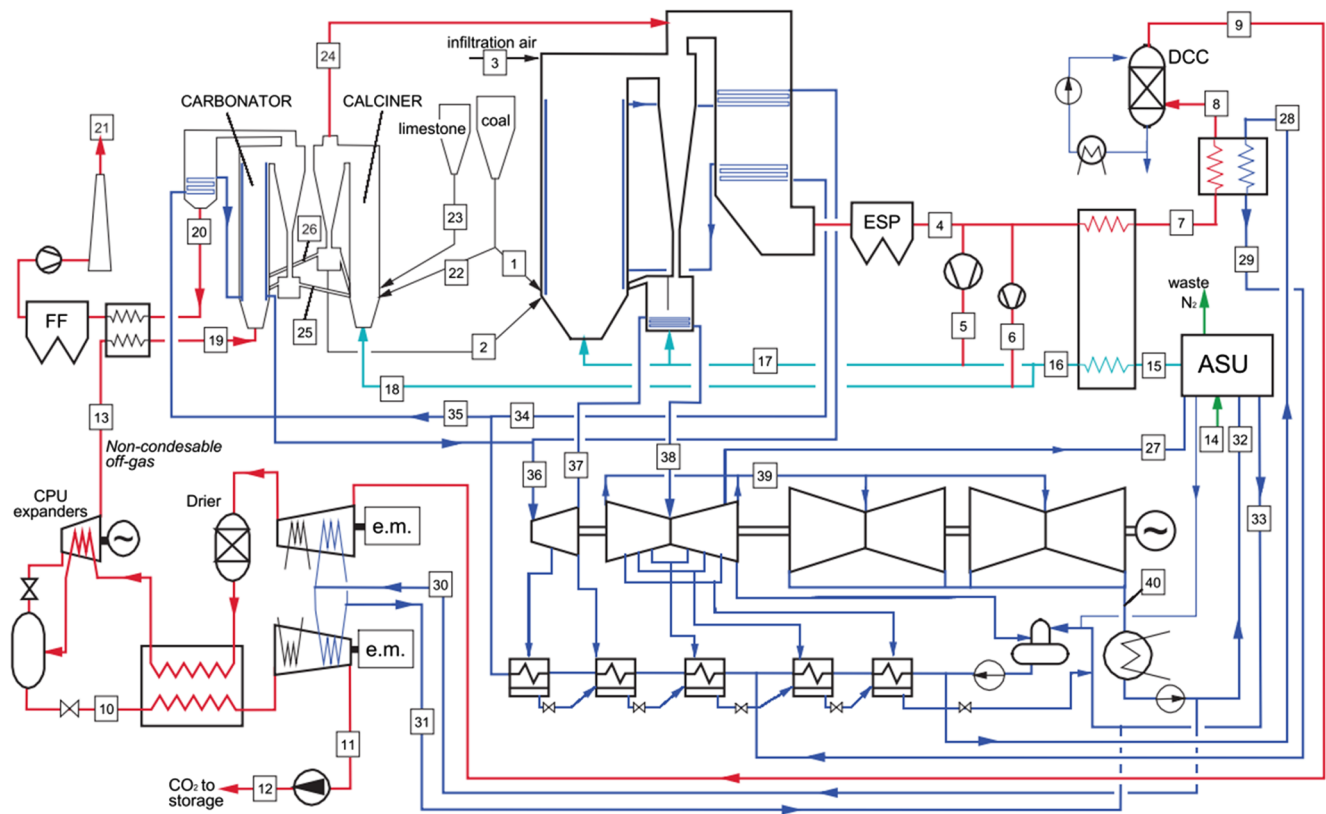


Fig. 10. Conceptual design of circulating fluidised bed oxy-fuel ultra-supercritical power plant with carbonate looping (Reprinted with permission from Romano [99]. Copyright 2013 Elsevier.)

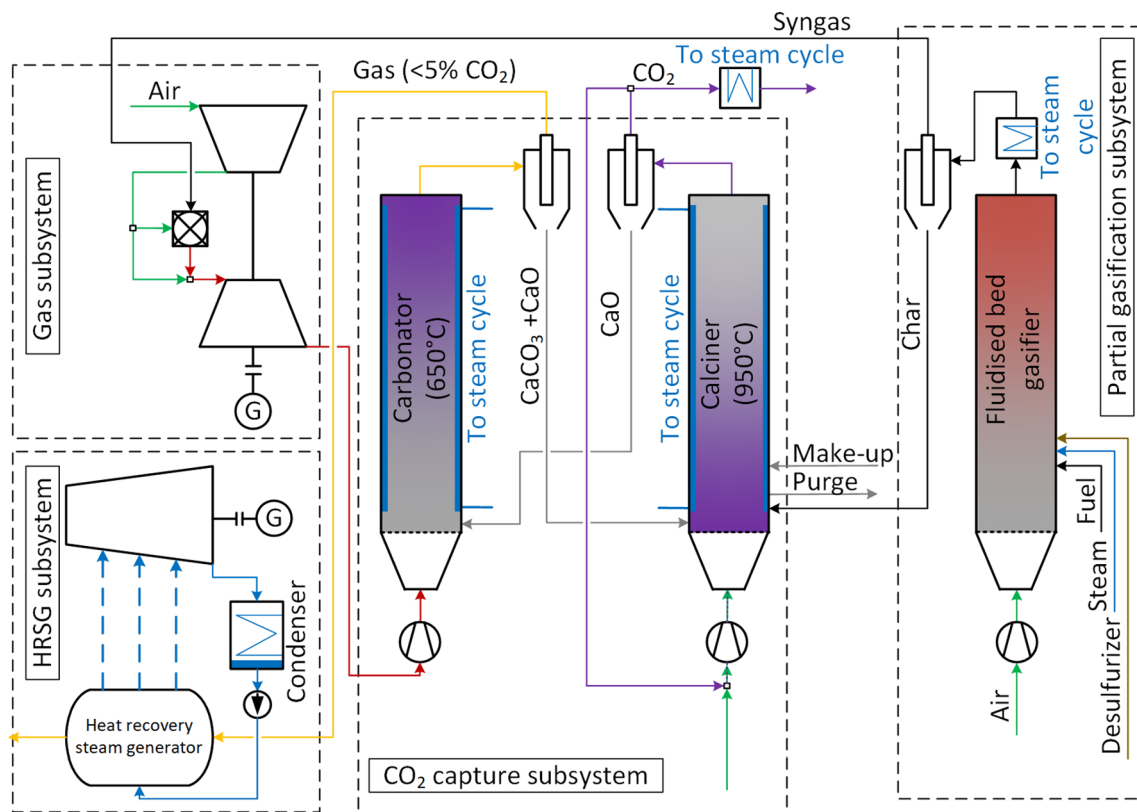


Fig. 11. Main components of the integrated gasification combined cycle power plant with carbonate looping for CO₂ capture (Adapted with permission from Li et al. [101]. Copyright 2011 Wiley.).

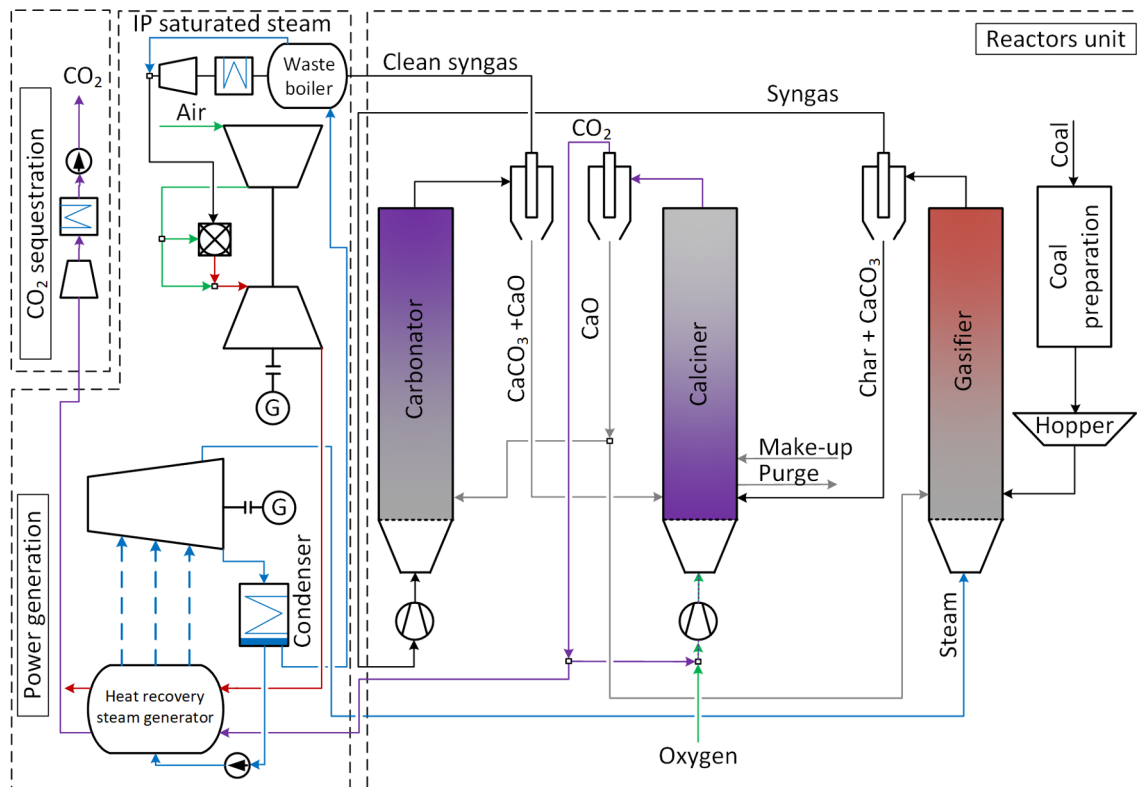


Fig. 12. Conceptual design of integration of carbonate looping plant to integrated-gasification combined cycle power plant (Adapted with permission from Wang et al. [105]. Copyright 2013 Elsevier.).

sub-critical steam cycle. The thermodynamic performance of this hydrogen-fueled IGCC power plant was characterised with a net efficiency between 41.0 and 45.4%, depending on the coal conversion in the

gasifier and the turbine inlet conditions, and a CO₂ capture level of 95%. This was found to be superior to conventional IGCC systems and supercritical CFPPs retrofitted with the ammonia-based CO₂ capture

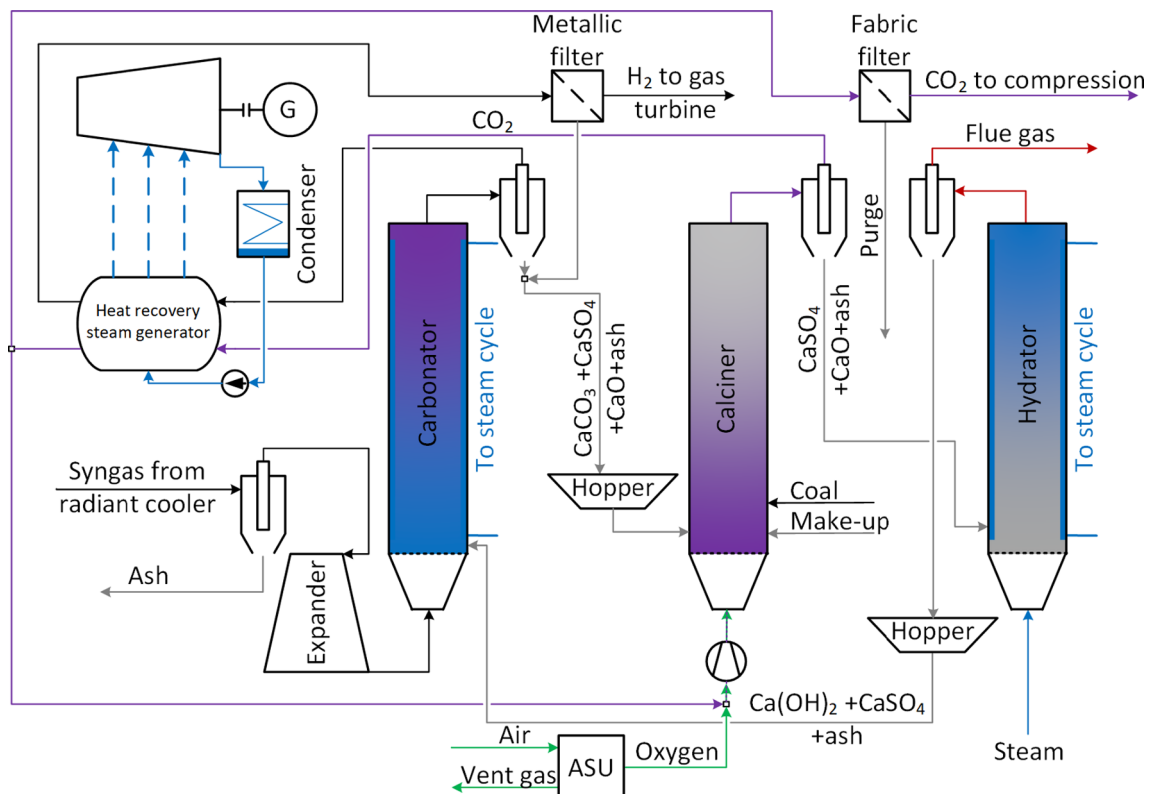


Fig. 13. Conceptual design of integration of carbonate looping plant to integrated-gasification combined cycle power plant (Adapted with permission from Connell et al. [109]. Copyright 2013 Elsevier.).

in a supercritical steam cycle for power generation. From the thermodynamic perspective, implementation of CaL and an oxygen-transfer membrane resulted in a net efficiency of 43.2%. This was found to be 3.8% points higher than that of conventional IGCC with an acid-gas removal system. It needs to be highlighted that such net efficiencies were in the range for the supercritical CFPPs without CO₂ capture [112,113]. For this reason, IGCC plants with CaL could be a feasible option for low-carbon power generation from coal that will be characterised by higher reliability compared the conventional IGCC due to the lack of a complicated chemical island.

As has been identified in Section 3, use of alternative sorbents may improve the performance of CaL-based systems [34,35,46,66]. Chi et al. [114] evaluated the effect of using CaO and sodium carbonate promoted magnesium oxide (Na₂CO₃-MgO) sorbent on the thermodynamic performance of a number of IGCC power plant configurations. The gasification island considered an oxygen-blown transport gasifier for syngas production, with the high-purity oxygen stream from a cryogenic ASU. The quality of syngas was further improved by considering either conventional two-stage water-gas shift, in which case CaL was located right after the shift reactors, or the sorption-enhanced water-gas shift (SEWGS) process. The cleaned syngas was then utilised in an F-class gas turbine and the high-grade heat utilised in a sub-critical steam cycle. In addition, similarly to the concept evaluated by Kunze et al. [111], part of the syngas stream was oxy-combusted in the calciner for sorbent regeneration. The thermodynamic assessment indicated that, if the conventional two-stage water-gas shift process was employed, the net efficiency of the IGCC with CaL was 36.7% and 37.5% if Na₂CO₃-MgO and CaO were used as a sorbent, respectively. The net efficiency in both cases was increased to 37.3% and 38.1%, if the SEWGS was considered. Poorer performance of the system using Na₂CO₃-MgO was primarily associated with lower temperature in the carbonator (400 °C) and the calciner (680 °C) for that sorbent. This led to less high-grade heat for recovery, and thus less additional power generated. Moreover,

the specific heat requirement for Na₂CO₃-MgO sorbent regeneration was found to be higher than that for CaO sorbent for sorbent conversions below 53%. As the conversions in CaL can vary between 15% [31] and 35% [46], depending on the sorbent degradation and fresh sorbent make-up rate, and considering the fact that the cost of MgO is one order of magnitude higher than that of CaO [115], use of that sorbent cannot be regarded as either technically or economically substantiated.

Another option to improve the performance of the novel gasification-based systems would be to consider alternative power islands that would be characterised with higher efficiencies. Romano and Lozza [116,117] have evaluated the thermodynamic performance of IGCC concepts that utilise CaL both as a pre-combustion CO₂ capture technology and as a heat source for power generation. Both zero-emissions coal mixed technology (ZECOMIX) [117] (Fig. 15) and zero-emissions coal mixed technology with air gas turbine (ZECOMAG) [116] (Fig. 16) can be divided into four sections – chemical island, oxygen island, CO₂ island and power island – and they only differ in the power island configuration. In the chemical island coal slurry is gasified under a hydrogen atmosphere in a hydrogasifier producing syngas that is then shifted to the hydrogen-rich stream in the carbonator. A small amount of oxygen is utilised to sustain the desired operating temperature at 700–1000 °C, depending on the operating pressure, ranging between 30 bar and 70 bar. A fraction of the hydrogen-rich stream is recycled from the carbonator to the hydrogasifier. The power island of ZECOMIX technology comprises a semi-closed Joule cycle, in which flue gas from the syngas oxy-combustion and the combustion gases are mixed with compressed steam to control the combustor outlet temperature. This mixture is expanded in a high-temperature steam turbine and then used for supercritical steam generation in the bottoming steam cycle [117]. Conversely, ZECOMAG technology has a more conventional power island, in which the syngas is burned with air in an open gas turbine cycle, and the discharged flue gas is used to generate supercritical steam in the dual-pressure heat recovery steam generator for the steam

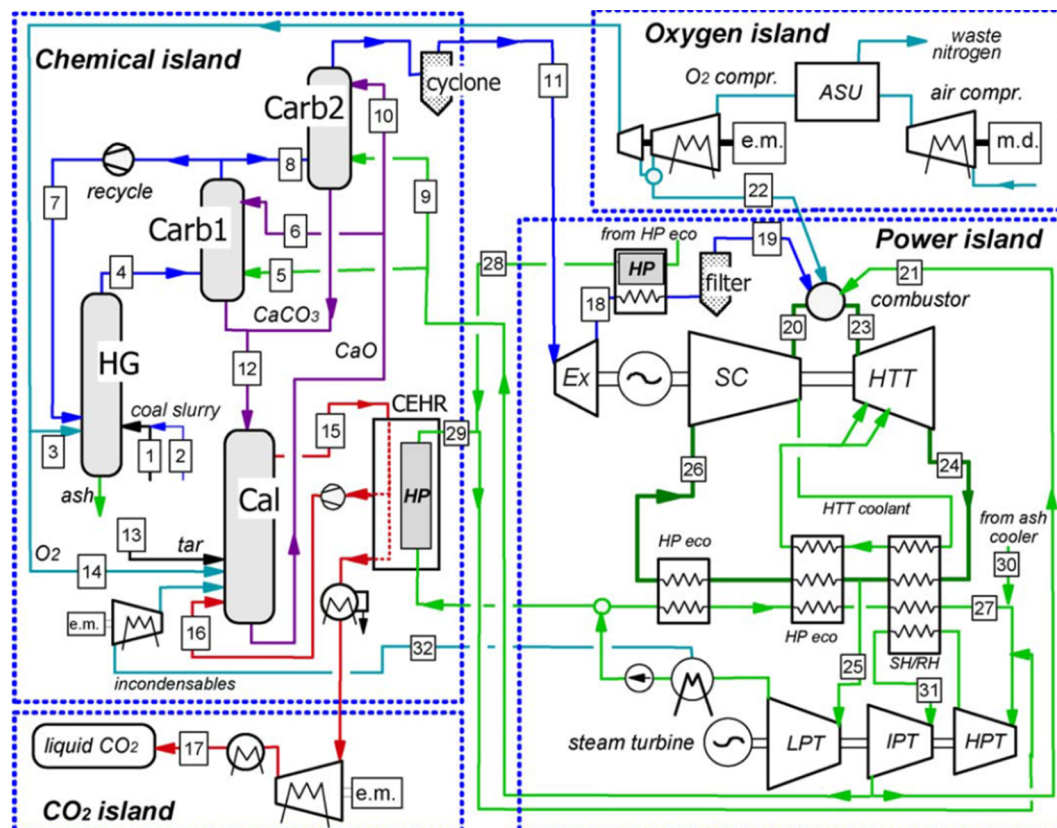


Fig. 15. Conceptual design of Zero-Emissions COal MIXed technology (Reprinted with permission from Romano and Lozza [117]. Copyright 2010 Elsevier.)

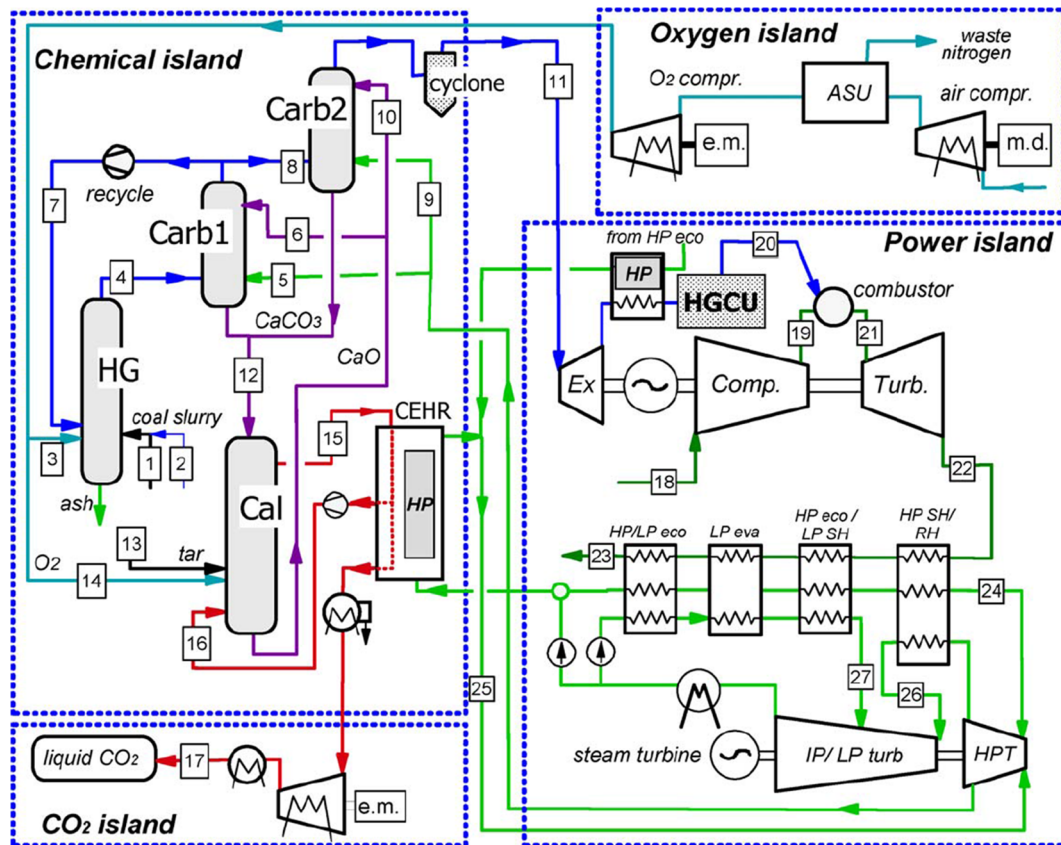


Fig. 16. Conceptual design of Zero-Emissions COal Mixed technology with Air Gas turbine (Reprinted with permission from Romano and Lozza [116]. Copyright 2010 Elsevier.)

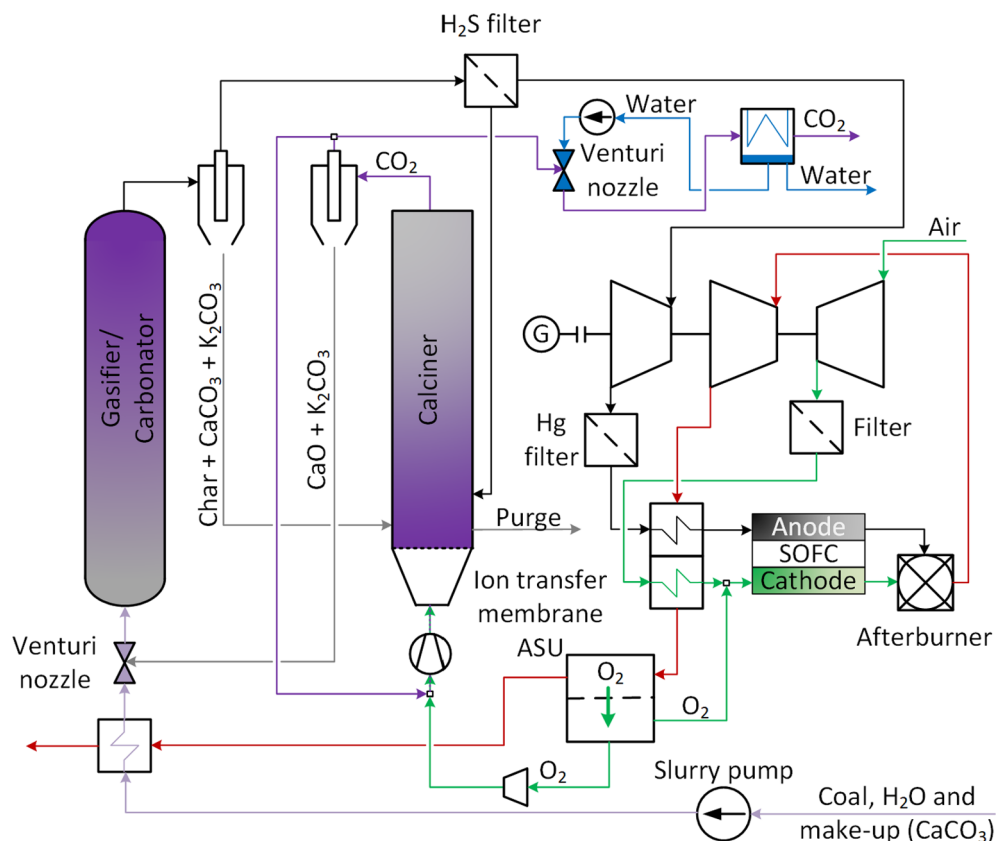


Fig. 17. Conceptual design of integrated-gasification fuel cell power plant (Adapted with permission from Siefert et al. [118]. Copyright 2014 Elsevier.).

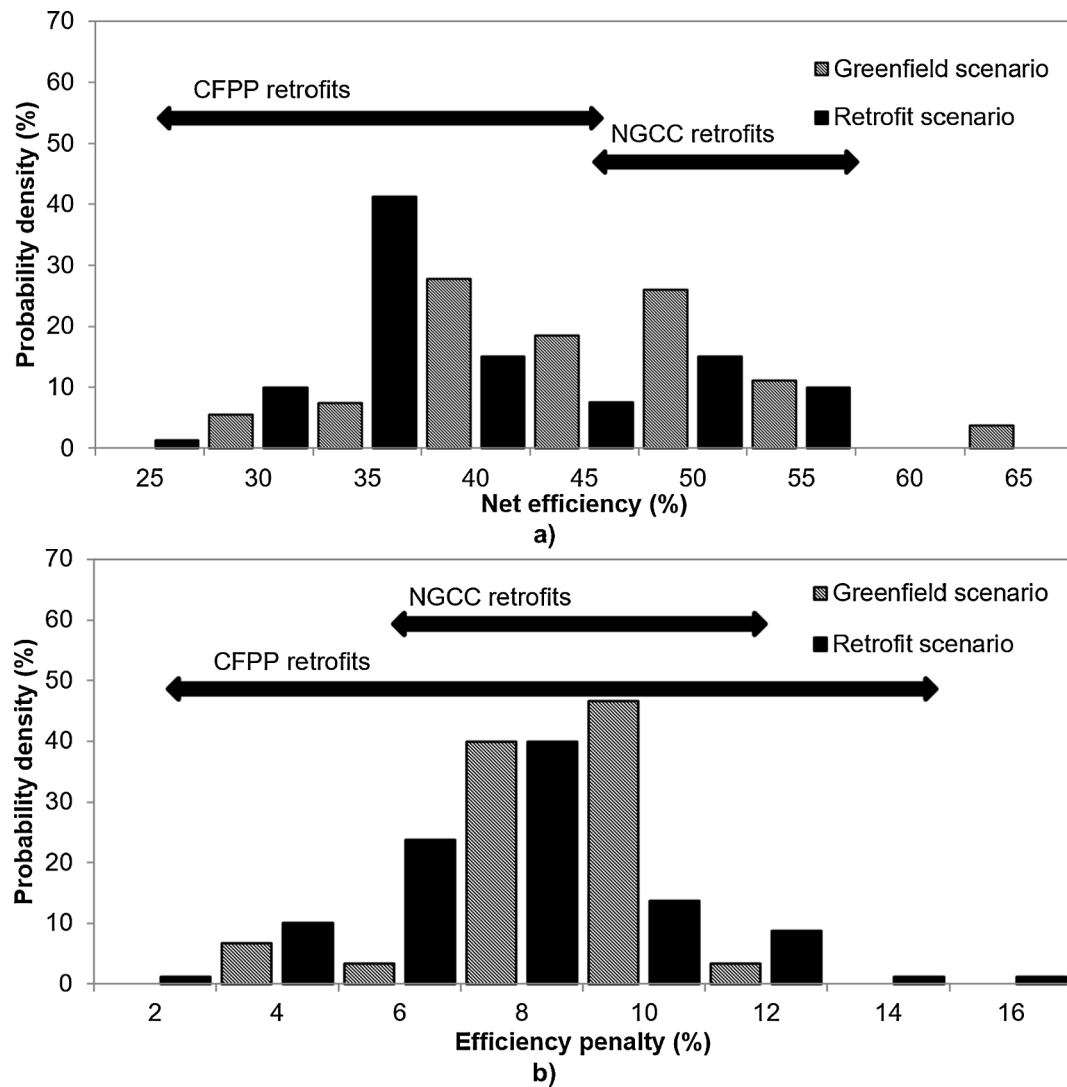


Fig. 21. Distribution of the (a) net efficiency and (b) efficiency penalty in the reviewed carbonate looping concepts.

high-efficiency and low CO₂ emissions. These have been classified as combustion-, gasification-, and reforming-based systems that were reported to achieve net efficiencies ranging between 28.6 and 60.6% with the mode and median equal to 51% and 42.6%, respectively (Fig. 21a). This indicates that such concepts may achieve higher net efficiencies than NGCCs (34–53%) in the existing fossil fuel-fired power plant fleet [128,129], but at considerably smaller environmental impact. Depending on the type of fuel used in the system and its thermochemical conversion technology, the most often-reported net efficiency of greenfield power generation systems ranges between 35% and 40% (CaL-based CFPPs), and 45% and 50% (integrated gasification and sorption-enhanced reforming-based power plants). The CaL-based CFPPs based on hybridising oxy-combustion with CaL were shown to result in net efficiencies of 28.6–37.4% with efficiency penalties between 7 and 9.2% points. Such performance is comparable to the CFPP retrofit scenarios reviewed in Section 3.1. The main benefit of such hybrid concepts, however, is the higher CO₂ capture level that can reach close to 99%. Conversely, the concepts based on the CaL process were reported to reach net efficiencies of 34.9–40.2% and result in efficiency penalties of 2.4–4.4% points. As the performance of these concepts can be further improved utilising the measures reported in Section 3, such as increase in the degree of heat integration or utilisation of higher-efficiency power cycles, the CaL-based CFPPs can be seen as feasible options to replace the existing unabated CFPPs in the mid-

term. The CaL-based IGCCs, in which coal or biomass is first converted into syngas and then utilised in the combined cycle, were reported to achieve net efficiencies ranging between 33.1 and 60.2%. The information on the efficiency penalty was found to be limited, as it was only reported by Cormos and Cormos [104], Cormos [102], and Chi et al. [114]. These studies indicated that the net efficiency of CaL-based IGCCs would be lower by 6.4–10.2% than the corresponding efficiency of conventional IGCCs. Nevertheless, most of the concepts presented in the current literature were reported to result in net efficiencies higher than 40%. Importantly, where the IGCC included the SOFC in addition to the gas turbine, the net efficiency was reported to be between 46.4 and 60.2%, even if biomass was used in syngas production. Such net efficiencies are considerably higher compared to those reported for novel combustion-based CFPPs in Section 4.1 (28.6–40.2%) and for existing unabated CFPPs (27–43%) reported in the literature [128,129]. Importantly, the IGCC concept utilising SOFC may even result in higher net efficiencies than those of the existing unabated NGCCs (34–53%). The CaL-based SESR concepts, in which natural gas was reformed into high-purity hydrogen and then utilised in a gas turbine and/or SOFC, were reported to achieve similar performance to CaL-based IGCCs, as their net efficiencies were reported to be between 42.3 and 60.2%. A study by Martinez et al. [90] compared the thermodynamic performance of CaL-based NGCC-SESR with the conventional NGCC without CO₂ capture, and indicated that the net efficiency of such a novel

concept would vary between 48.9 and 51.0%, resulting in an efficiency penalty ranging between 7.8 and 9.9%. Although the CaL-based SESR concepts produce high-purity hydrogen, linking them with standalone SOFCs was shown to yield net efficiencies of 42.3–51%. This is at best comparable to the CaL-based NGCC-SESR concepts that utilise conventional NGCC architecture. Importantly, the CaL-based SESR concepts that combine SOFC with another power cycle were shown to achieve a net efficiency of 60.2%. It needs to be highlighted that in contrast to the CaL-based IGCCs, all proposed CaL-based SESR concepts result in net efficiencies higher than 40%, and most of them achieve net efficiencies around 45–50% with the potential to reach 60%. Such figures are comparable to those reported for existing unabated NGCCs (43–58%) [132], indicating that CaL-based SESR concepts could offer comparable thermodynamic performance to existing systems, but at a much lower environmental impact. Overall, it can be noted that the net efficiencies reported for the greenfield scenarios are higher compared to those for the retrofit scenarios. This indicates that the CaL-based power generation systems could be implemented in place of the existing fleet of conventional fossil fuel power plants, leading to both increased average net fleet efficiency and substantial reduction in its carbon intensity.

6. Economic feasibility assessment

As opposed to the thermodynamic feasibility assessments, the data supporting the economic feasibility of the CaL concepts appears to be limited in the current literature, especially for the greenfield scenarios. Therefore, the thermodynamic feasibility of the CaL-based power generation systems still needs to be substantiated via their economic feasibility.

The current literature most often report that retrofit of CaL to fossil fuel-fired power generation systems will result in LCOEs between 50 and 75 €/MWh (Fig. 22a), and the cost of CO₂ avoided (AC) was most often reported to be between 10 and 30 €/tCO₂ (Fig. 22b), regardless of whether CaL was retrofitted to NGCC or CFPP. Such economic performance has been shown to be superior to chemical solvent scrubbing (LCOE = 65–89 €/MWh; AC = 35–75 €/tCO₂) [73,75–78] and oxy-fuel combustion (LCOE = 55–75 €/MWh; AC = 35–75 €/tCO₂) [135,136] retrofits.

As indicated above, a limited amount of data have been presented in the current literature on the economic performance of CaL-based power generation systems. These data indicate that the LCOE and the cost of CO₂ avoided associated with the greenfield scenarios are most likely to be within 50–100 €/MWh and 10–50 €/tCO₂, respectively (Fig. 22).

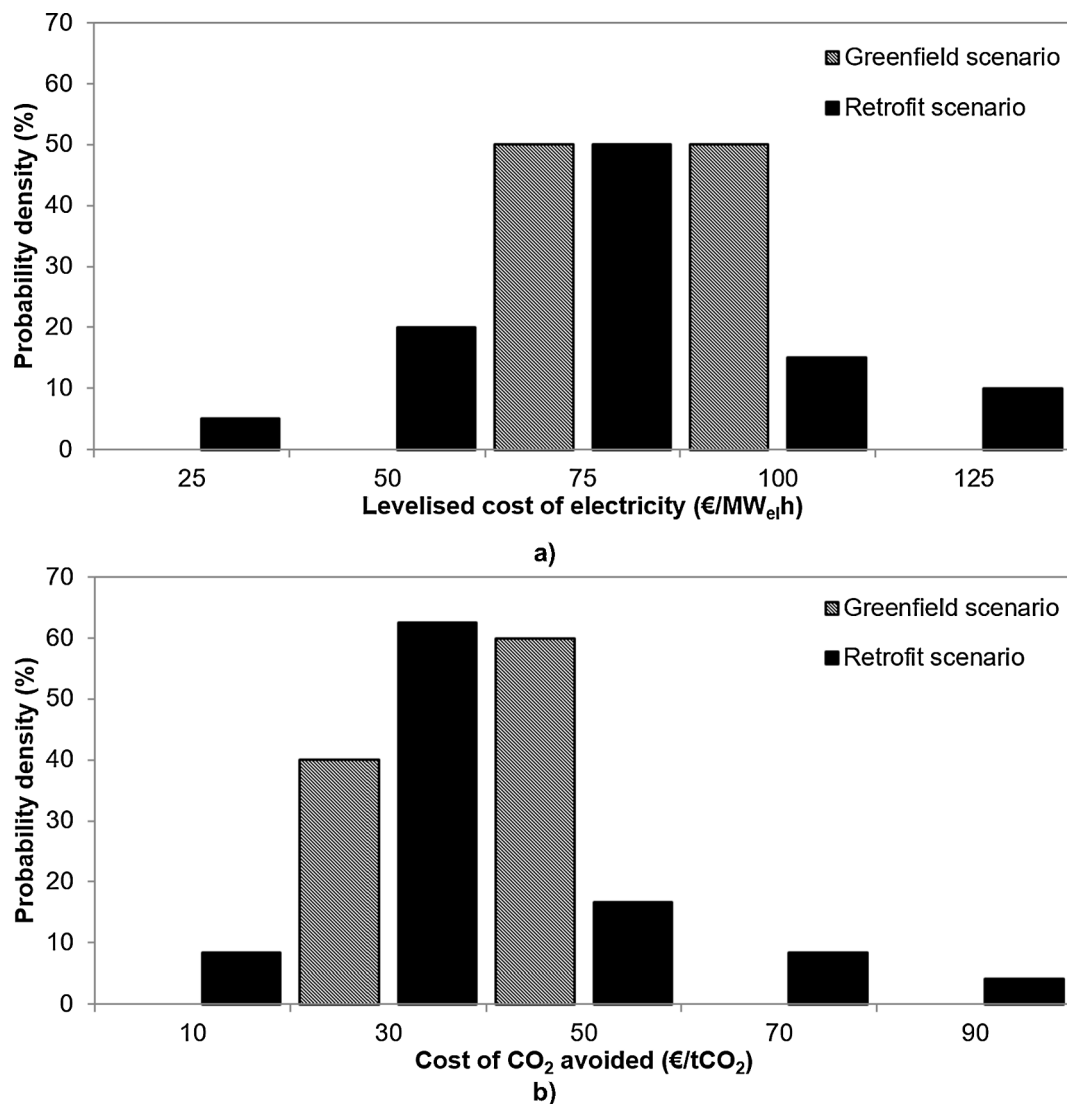


Fig. 22. Distribution of the (a) levelised cost of electricity, (b) cost of CO₂ avoided in the reviewed carbonate looping concepts.

Although such economic performance appears to be competitive to that reported for the retrofit scenarios, economic feasibility of such novel concepts must be further proven to substantiate their competitive thermodynamic performance assessed in Section 5. It also needs to be highlighted that, although alternative sorbents may be characterised with lower degradation than natural sorbents, their high price may make them not economically feasible [68]. Therefore, it is pertinent that the optimisation and development of CaL-based power generation systems are supported by both thermodynamic and economic feasibility assessment. Finally, the economic assessments presented in the current literature are mostly based on deterministic models that do not account for the uncertainty in the operating conditions of CaL and the market conditions. As indicated by Hanak and Manovic [69], the most probable values of the LCOE in the CaL retrofit to CFPPs will be between 75 and 115 €/MWh. As this range is higher than that identified using the deterministic models, it is pertinent to consider the effect of uncertainty on the economic performance.

7. Perspective for carbonate looping cycles

Timely decarbonisation of the power sector is crucial to meeting a challenging emission reduction target set out by the Paris Agreement. Such transformation of this sector can only be achieved via wide implementation of low-carbon power generation concepts, including novel power generation systems with CCS. However, the most mature technologies, such as chemical solvent scrubbing and oxy-combustion, impose a significant thermodynamic and economic burden on retrofitting to existing fossil fuel-fired power generation systems. CaL has been shown to be a feasible technology that, when optimised, has the potential to ensure low-carbon power generation at an affordable cost.

The current literature presents a wide number of CaL concepts for decarbonisation of fossil fuel-fired power generation systems that can be broadly classified into retrofit and greenfield scenarios. Retrofits of CaL concepts to existing fossil fuel-fired power plants have been shown to result in efficiency penalties between 6 and 8% points, with net efficiencies varying between 24 and 44% for CFPP and 45–53% for NGCC retrofits. However, considering a large number of alternative CaL configurations and more stable sorbents, the potential exists to reduce the efficiency penalty to below 5% points. This would not only lead to improved economic performance of the entire system, but also to reduced GHG emissions over its lifetime. Furthermore, the CaL-based power generation systems have been shown to be most likely to achieve net efficiencies as high as 40% for CaL-based CFPPs and 50% for CaL-based IGCC and SESR power plants. Yet, similarly to the retrofit scenarios, there is still the potential for further improvement of their thermodynamic performance via increased degree of heat integration and/or utilisation of higher efficiency power cycles. Overall, the net efficiencies reported for the greenfield scenarios are higher than for the retrofit scenarios. Therefore, CaL-based power generation systems could be implemented in place of the existing fleet of conventional fossil fuel power plants, which contains a large share of subcritical CFPPs characterised with net efficiencies lower than 33%, resulting in both increased average net fleet efficiency and substantial reduction in the carbon intensity.

Importantly, the current literature presents limited information on the economic feasibility assessment of CaL concepts, especially for the greenfield scenarios. The cost of CO₂ avoided has been shown to be between 10 and 30 €/tCO₂ and 10–50 €/tCO₂ in the retrofit and greenfield scenarios, respectively. Such economic performance has been shown to be superior to that of chemical solvent scrubbing (AC = 35–75 €/tCO₂) and oxy-fuel combustion (AC = 35–75 €/tCO₂) retrofits, as the costs associated with CO₂ capture using CaL were shown to be nearly half that of mature CCS technologies.

Nevertheless, a vast majority of the assessments of the CaL-based power generation systems included only thermodynamic analyses, and lacked any indication about potential improvements to the economic

performance. It needs to be stressed that the improvements in the thermodynamic performance of such processes, achieved as a result of novel process configuration development and application of more durable sorbents, needs to be substantiated by the economic analysis. This is particularly important regarding sorbents, as regardless of lower degradation, the novel sorbents may be characterised with a high price making the entire process not economically feasible. Finally, existing assessments of the economic feasibility of CaL concepts are based on deterministic models that do not account for uncertainty in the operating conditions of CaL and the market conditions. To account for uncertainty and increase the reliability of the predictions, it is pertinent to incorporate a stochastic approach into the economic assessment.

Overall, the current reading of CaL-based power generation systems indicates that these have significant potential to achieve net efficiencies above 50%, especially if the process includes SOFC, at near-zero (10 gCO₂/kWh) or negative (biomass-fired systems) CO₂ emissions. Such performance can be seen as competitive to the state-of-the-art NGCCs without CO₂ capture, implying that wide deployment of CaL-based power generation systems, especially IGCCs and SESR-based power plants, would result in decarbonisation of the power sector with no energy penalty. Importantly, the existing fleet comprises a large share of subcritical units that operate with the net efficiencies lower than 33%. Therefore, not only can a substantial reduction in the carbon intensity of the power plant fleet be achieved, but also there is the potential for an improvement in the average net fleet efficiency. It is critical, however, to assess the economic performance of CaL-based power generation systems to substantiate their thermodynamic performance and benchmark their attractiveness to the market.

8. Conclusions

CaL is often regarded as an emerging CO₂ capture technology that can reduce economic and efficiency penalties associated with more mature technologies. Its maturity has increased significantly over the past twenty years, mostly due to development of novel process configurations and sorbents for improved process performance. This review aimed to provide a comprehensive overview of CaL concepts and statistically assess their techno-economic feasibility based on the evidence published in the literature. It has been shown that:

- CaL can both be efficiently retrofitted to existing fossil fuel-fired power generation systems and be the basis for development of novel greenfield power generation systems;
- CaL retrofits have most commonly been reported to result in efficiency penalties between 6 and 8% points when retrofitted to existing fossil fuel-fired power generation systems;
- CaL-based greenfield power generation systems can achieve net efficiencies as high as 40–60% at near-zero CO₂ emissions, especially when sorption-enhanced hydrogen production and SOFC are considered;
- a number of measures for net efficiency improvements have been proposed, including increased degree of heat integration, using advanced power cycles, and advanced CaL configurations;
- the cost of CO₂ avoided associated with CaL is 10–50 €/tCO₂ and is superior to that of chemical solvent scrubbing and oxy-fuel combustion; and
- improvements in thermodynamic performance are not always supported by economic assessments.

Acknowledgements

This publication is based on research conducted within the “Redefining power generation from carbonaceous fuels with carbonate looping combustion and gasification technologies” project funded by UK Engineering and Physical Sciences Research Council (EPSRC reference: EP/P034594/1). Data underlying this study can be accessed

through the Cranfield University repository at 10.17862/cranfield.rd.7128053.

References

- [1] IEA. Energy climate change and environment. Paris, France: IEA Publications; 2016.
- [2] Tollefson J. Is the 2°C world a fantasy? *Nature* 2015;527:436–8. <https://doi.org/10.1038/527436a>.
- [3] IEA. 20 years of carbon capture and storage. Accelerating future deployment. Paris, France: IEA Publications; 2016.
- [4] IEA. Tracking Clean Energy Progress 2017. Energy Technology Perspectives 2017 Excerpt. Informing Energy Sector Transformations. Paris, France: IEA Publications; 2017.
- [5] DECC. CCS Roadmap. Supporting deployment of carbon capture and storage in the UK. London, UK: Department of Energy and Climate Change; 2012.
- [6] Boot-Handford ME, Abanades JC, Anthony EJ, Blunt MJ, Brandani S, Mac Dowell N, et al. Carbon capture and storage update. *Energy Environ Sci* 2014;7:130–89. <https://doi.org/10.1039/C3EE42350F>.
- [7] Hanak DP, Anthony EJ, Manovic V. A review of developments in pilot plant testing and modelling of calcium looping process for CO₂ capture from power generation systems. *Energy Environ Sci* 2015;8:2199–249. <https://doi.org/10.1039/C5EE01228G>.
- [8] Renner M. Carbon prices and CCS investment: a comparative study between the European Union and China. *Energy Policy* 2014;75:327–40. <https://doi.org/10.1016/j.enpol.2014.09.026>.
- [9] Supekar SD, Skerlos SJ. Reassessing the efficiency penalty from carbon capture in coal-fired power plants. *Environ Sci Technol* 2015;49:12576–84. <https://doi.org/10.1021/acs.est.5b03052>.
- [10] Singh B, Strømman AH, Hertwich EG. Comparative life cycle environmental assessment of CCS technologies. *Int J Greenh Gas Control* 2011;5:911–21. <https://doi.org/10.1016/j.jggc.2011.03.012>.
- [11] Koornneef J, van Keulen T, Faaij A, Turkenburg W. Life cycle assessment of a pulverized coal power plant with post-combustion capture, transport and storage of CO₂. *Int J Greenh Gas Control* 2008;2:448–67. <https://doi.org/10.1016/j.jggc.2008.06.008>.
- [12] Schlögl R, Abanades C, Aresta M, Blekkan MA, Cantat T, Centi G, et al. Novel carbon capture and utilisation technologies - research and climate aspects. Berlin, Germany: SAPEA; 2018.
- [13] Hiramata T, Hosoda H, Kitano K, Shimizu T. Method of separating carbon dioxide from carbon dioxide containing gas and combustion apparatus having function to separate carbon dioxide from the combustion gas. UK Patent 2291051A; 1996.
- [14] Shimizu T, Hiramata T, Hosoda H, Kitano K, Inagaki M, Tejima K. A twin fluid-bed reactor for removal of CO₂ from combustion processes. *Chem Eng Res Des* 1999;77:62–8. <https://doi.org/10.1205/026387699525882>.
- [15] Ströhle J, Junk M, Kremer J, Galloy A, Eppe B. Carbonate looping experiments in a 1 MW_{th} pilot plant and model validation. *Fuel* 2014;127:13–22. <https://doi.org/10.1016/j.fuel.2013.12.043>.
- [16] Arias B, Diego ME, Abanades JC, Lorenzo M, Diaz L, Martínez D, et al. Demonstration of steady state CO₂ capture in a 1.7MW_{th} calcium looping pilot. *Int J Greenh Gas Control* 2013;18:237–45. <https://doi.org/10.1016/j.jggc.2013.07.014>.
- [17] Chang M-H, Chen W-C, Huang C-M, Liu W-H, Chou Y-C, Chang W-C, et al. Design and experimental testing of a 1.9 MW_{th} calcium looping pilot plant. *Energy Proc* 2014;63:2100–8. <https://doi.org/10.1016/j.egypro.2014.11.226>.
- [18] Dean CC, Blamey J, Florin NH, Al-Jeboori MJ, Fennell PS. The calcium looping cycle for CO₂ capture from power generation, cement manufacture and hydrogen production. *Chem Eng Res Des* 2011;89:836–55. <https://doi.org/10.1016/j.cherd.2010.10.013>.
- [19] Florin NH, Harris AT. Enhanced hydrogen production from biomass with in situ carbon dioxide capture using calcium oxide sorbents. *Chem Eng Sci* 2008;63:287–316. <https://doi.org/10.1016/j.ces.2007.09.011>.
- [20] Perejón A, Romeo LM, Lara Y, Lisbona P, Martínez A, Valverde JM. The calcium-looping technology for CO₂ capture: on the important roles of energy integration and sorbent behavior. *Appl Energy* 2016;162:787–807. <https://doi.org/10.1016/j.apenergy.2015.10.121>.
- [21] Harrison DP. Sorption-enhanced hydrogen production: a review. *Ind Eng Chem Res* 2008;47:6486–501. <https://doi.org/10.1021/ie800298z>.
- [22] Erans M, Manovic V, Anthony EJ. Calcium looping sorbents for CO₂ capture. *Appl Energy* 2016;180:722–42. <https://doi.org/10.1016/j.apenergy.2016.07.074>.
- [23] Kierzkowska AM, Pacciani R, Müller CR. CaO-based CO₂ sorbents: from fundamentals to the development of new, highly effective materials. *ChemSusChem* 2013;6:1130–48. <https://doi.org/10.1002/cssc.201300178>.
- [24] Liu W, An H, Qin C, Yin J, Wang G, Feng B, et al. Performance enhancement of calcium oxide sorbents for cyclic CO₂ capture - a review. *Energy Fuels* 2012;26:2751–67. <https://doi.org/10.1021/ef300220x>.
- [25] Blamey J, Anthony EJ, Wang J, Fennell PS. The calcium looping cycle for large-scale CO₂ capture. *Prog Energy Combust Sci* 2010;36:260–79. <https://doi.org/10.1016/j.peccs.2009.10.001>.
- [26] Anthony EJ. Ca looping technology: Current status, developments and future directions. *Greenh Gases Sci Technol* 2011;1:36–47. <https://doi.org/10.1002/ghg3.2>.
- [27] Stanmore BR, Gilot P. Review—calcination and carbonation of limestone during thermal cycling for CO₂ sequestration. *Fuel Process Technol* 2005;86:1707–43. <https://doi.org/10.1016/j.fuproc.2005.01.023>.
- [28] Romano MC, Martínez I, Murillo R, Arstad B, Blom R, Özcan DC, et al. Process simulation of Ca-looping processes: review and guidelines. *Energy Proc* 2013;37:142–50. <https://doi.org/10.1016/j.egypro.2014.11.239>.
- [29] Martínez I, Grasa G, Parkkinen J, Tynjälä T, Hyppänen T, Murillo R, et al. Review and research needs of Ca-looping systems modelling for post-combustion CO₂ capture applications. *Int J Greenh Gas Control* 2016;50:271–304. <https://doi.org/10.1016/j.jggc.2016.04.002>.
- [30] Hughes RW, Lu DY, Anthony EJ, Macchi A. Design, process simulation and construction of an atmospheric dual fluidized bed combustion system for in situ CO₂ capture using high-temperature sorbents. *Fuel Process Technol* 2005;86:1523–31. <https://doi.org/10.1016/j.fuproc.2005.01.006>.
- [31] Hanak DP, Biliyok C, Anthony EJ, Manovic V. Modelling and comparison of calcium looping and chemical solvent scrubbing retrofits for CO₂ capture from coal-fired power plant. *Int J Greenh Gas Control* 2015;42:226–36. <https://doi.org/10.1016/j.jggc.2015.08.003>.
- [32] Winkler HGF. Petrogenesis of metamorphic rocks. Berlin, Germany: Springer; 1976.
- [33] Oates JAH. Lime and Limestone, Chemistry and Technology, Production and Uses. Weinheim, Germany: Wiley-VCH; 1998.
- [34] Wang W, Ramkumar S, Wong D, Fan L. Simulations and process analysis of the carbonation-calcination reaction process with intermediate hydration. *Fuel* 2012;92:94–106. <https://doi.org/10.1016/j.fuel.2011.06.059>.
- [35] Wang W, Ramkumar S, Fan L. Energy penalty of CO₂ capture for the carbonation-calcination reaction (CCR) process: parametric effects and comparisons with alternative processes. *Fuel* 2013;104:561–74. <https://doi.org/10.1016/j.fuel.2012.04.043>.
- [36] Hanak DP, Manovic V. Calcium looping combustion for high-efficiency low-emission power generation. *J Clean Prod* 2017;161:245–55. <https://doi.org/10.1016/j.jclepro.2017.05.080>.
- [37] Abanades JC, Murillo R, Fernandez JR, Grasa G, Martínez I. New CO₂ capture process for hydrogen production combining Ca and Cu chemical loops. *Environ Sci Technol* 2010;44:6901–4. <https://doi.org/10.1021/es101707t>.
- [38] Duhoux B, Mehrani P, Lu DY, Symonds RT, Anthony EJ, Macchi A. Combined calcium looping and chemical looping combustion for post-combustion carbon dioxide capture: process simulation and sensitivity analysis. *Energy Technol* 2016;4:1–14. <https://doi.org/10.1002/ente.201600024>.
- [39] Özcan DC, Macchi A, Lu DY, Kierzkowska AM, Ahn H, Müller CR, et al. Ca–Cu looping process for CO₂ capture from a power plant and its comparison with Ca-looping, oxy-combustion and amine-based CO₂ capture processes. *Int J Greenh Gas Control* 2015;43:198–212. <https://doi.org/10.1016/j.jggc.2015.10.021>.
- [40] Manovic V, Anthony EJ. Integration of calcium and chemical looping combustion using composite CaO/CuO-based materials. *Environ Sci Technol* 2011;45:10750–6. <https://doi.org/10.1021/es202292c>.
- [41] Martínez I, Murillo R, Grasa G, Rodríguez N, Abanades JC. Conceptual design of a three fluidised beds combustion system capturing CO₂ with CaO. *Int J Greenh Gas Control* 2011;5:498–504. <https://doi.org/10.1016/j.jggc.2010.04.017>.
- [42] Abanades JC, Anthony EJ, Wang J, Oakey JE. Fluidized bed combustion systems integrating CO₂ capture with CaO. *Environ Sci Technol* 2005;39:2861–6. <https://doi.org/10.1021/es049622t>.
- [43] Moon H, Yoo H, Seo H, Park YK, Cho HH. Thermal design of heat-exchangeable reactors using a dry-sorbent CO₂ capture multi-step process. *Energy* 2015;84:704–13. <https://doi.org/10.1016/j.energy.2015.03.034>.
- [44] Junk M, Reitz M, Ströhle J, Eppe B. Technical and economical assessment of the indirectly heated carbonate looping process. *J Energy Resour Technol* 2016;138:042210. <https://doi.org/10.1115/1.4033142>.
- [45] Junk M, Reitz M, Ströhle J, Eppe B. Thermodynamic evaluation and cold flow model testing of an indirectly heated carbonate looping process. *Chem Eng Technol* 2013;36:1479–87. <https://doi.org/10.1002/ceat.201300019>.
- [46] Berstad D, Anantharaman R, Blom R, Jordal K, Arstad B. NGCC post-combustion CO₂ capture with Ca/carbonate looping: efficiency dependency on sorbent properties, capture unit performance and process configuration. *Int J Greenh Gas Control* 2014;24:43–53. <https://doi.org/10.1016/j.jggc.2014.02.015>.
- [47] Romeo LM, Abanades JC, Escosa JM, Paño J, Giménez A, Sánchez-Biezma A, et al. Oxyfuel carbonation/calcination cycle for low cost CO₂ capture in existing power plants. *Energy Convers Manag* 2008;49:2809–14. <https://doi.org/10.1016/j.enconman.2008.03.022>.
- [48] Hanak DP, Erans M, Nabavi SA, Jeremias M, Romeo LM, Manovic V. Technical and economic feasibility evaluation of calcium looping with no CO₂ recirculation. *Chem Eng J* 2018;335:763–73. <https://doi.org/10.1016/j.ces.2017.11.022>.
- [49] Hawthorne C, Trossmann M, Galindo Cifre P, Schuster A, Scheffknecht G. Simulation of the carbonate looping power cycle. *Energy Proc* 2009;1:1387–94. <https://doi.org/10.1016/j.egypro.2009.01.182>.
- [50] Ströhle J, Lasheras A, Galloy A, Eppe B. Simulation of the carbonate looping process for post-combustion CO₂ capture from a coal-fired power plant. *Chem Eng Technol* 2009;32:435–42. <https://doi.org/10.1002/ceat.200800569>.
- [51] Ströhle J, Galloy A, Eppe B. Feasibility study on the carbonate looping process for post-combustion CO₂ capture from coal-fired power plants. *Energy Proc* 2009;1:1313–20. <https://doi.org/10.1016/j.egypro.2009.01.172>.
- [52] Lasheras A, Ströhle J, Galloy A, Eppe B. Carbonate looping process simulation using a 1D fluidized bed model for the carbonator. *Int J Greenh Gas Control* 2011;5:686–93. <https://doi.org/10.1016/j.jggc.2011.01.005>.
- [53] Martínez I, Murillo R, Grasa G, Carlos Abanades J. Integration of a Ca looping system for CO₂ capture in existing power plants. *AIChE J* 2011;57:2599–607. <https://doi.org/10.1002/aic.12461>.
- [54] Hanak DP, Biliyok C, Manovic V. Efficiency improvements for the coal-fired power

- plant retrofit with CO₂ capture plant using chilled ammonia process. *Appl Energy* 2015;151:258–72. <https://doi.org/10.1016/j.apenergy.2015.04.059>.
- [55] Lara Y, Lisbona P, Martínez A, Romeo LM. Design and analysis of heat exchanger networks for integrated Ca-looping systems. *Appl Energy* 2013;111:690–700. <https://doi.org/10.1016/j.apenergy.2013.05.044>.
- [56] Lara Y, Lisbona P, Martínez A, Romeo LM. A systematic approach for high temperature looping cycles integration. *Fuel* 2014;127:4–12. <https://doi.org/10.1016/j.fuel.2013.09.062>.
- [57] Vorrías I, Atsonios K, Nikolopoulos A, Nikolopoulos N, Grammelis P, Kakaras E. Calcium looping for CO₂ capture from a lignite fired power plant. *Fuel* 2013;113:826–36. <https://doi.org/10.1016/j.fuel.2012.12.087>.
- [58] ECN. ECN Phyllis classification 2012. www.ecn.nl/phyllis2/Browse/Standard/ECN-Phyllis (accessed July 19, 2018).
- [59] Ortiz C, Chacartegui R, Valverde JM, Becerra JA. A new integration model of the calcium looping technology into coal fired power plants for CO₂ capture. *Appl Energy* 2016;169:408–20. <https://doi.org/10.1016/j.apenergy.2016.02.050>.
- [60] Martínez A, Lara Y, Lisbona P, Romeo LM. Energy penalty reduction in the calcium looping cycle. *Int J Greenh Gas Control* 2012;7:74–81. <https://doi.org/10.1016/j.ijggc.2011.12.005>.
- [61] Martínez A, Lara Y, Lisbona P, Romeo LM, Martínez A, Lara Y, et al. Operation of a cyclonic preheater in the Ca-looping for CO₂ capture. *Environ Sci Technol* 2013;47:11335–41. <https://doi.org/10.1021/es401601k>.
- [62] Arias B, Abanades JC, Grasa GS. An analysis of the effect of carbonation conditions on CaO deactivation curves. *Chem Eng J* 2011;167:255–61. <https://doi.org/10.1016/j.cej.2010.12.052>.
- [63] Hanak DP, Manovic V. Calcium looping with supercritical CO₂ cycle for decarbonisation of coal-fired power plant. *Energy* 2016;102:343–53. <https://doi.org/10.1016/j.energy.2016.02.079>.
- [64] Manovic V, Anthony EJ. Steam reactivation of spent CaO-based sorbent for multiple CO₂ capture cycles. *Environ Sci Technol* 2007;41:1420–5. <https://doi.org/10.1021/es0621344>.
- [65] Materic V, Symonds R, Lu D, Holt R, Manovic V. Performance of hydration reactivated Ca looping sorbents in a pilot-scale, oxy-fired dual fluid bed unit. *Energy Fuels* 2014;28:5363–72. <https://doi.org/10.1021/ef501203v>.
- [66] Hanak DP, Biliyok C, Manovic V. Calcium looping with inherent energy storage for decarbonisation of coal-fired power plant. *Energy Environ Sci* 2016;9:971–83. <https://doi.org/10.1039/C5EE02950C>.
- [67] Ortiz C, Valverde JM, Chacartegui R. Energy consumption for CO₂ capture by means of the calcium looping process: a comparative analysis using limestone, dolomite, and steel slag. *Energy Technol* 2016;4:1317–27. <https://doi.org/10.1002/ente.201600390>.
- [68] Lisbona P, Martínez A, Lara Y, Romeo LM. Integration of carbonate CO₂ capture cycle and coal-fired power plants. A comparative study for different sorbents. *Energy Fuels* 2010;24:728–36. <https://doi.org/10.1021/ef900740p>.
- [69] Hanak DP, Manovic V. Economic feasibility of calcium looping under uncertainty. *Appl Energy* 2017;208:691–702. <https://doi.org/10.1016/j.apenergy.2017.09.078>.
- [70] Abanades JC, Grasa G, Alonso M, Rodriguez N, Anthony EJ, Romeo LM. Cost structure of a postcombustion CO₂ capture system using CaO. *Environ Sci Technol* 2007;41:5523–7. <https://doi.org/10.1021/es070099a>.
- [71] Romano MC, Spinelli M, Campanari S, Consonni S, Cinti G, Marchi M, et al. The calcium looping process for low CO₂ emission cement and power. *Energy Proc* 2013;37:7091–9. <https://doi.org/10.1016/j.egypro.2013.06.645>.
- [72] Cormos CC. Economic evaluations of coal-based combustion and gasification power plants with post-combustion CO₂ capture using calcium looping cycle. *Energy* 2014;78:665–73. <https://doi.org/10.1016/j.energy.2014.10.054>.
- [73] Cormos AM, Cormos CC. Techno-economic evaluations of post-combustion CO₂ capture from sub- and super-critical circulated fluidised bed combustion (CFBC) power plants. *Appl Therm Eng* 2017;127:106–15. <https://doi.org/10.1016/j.applthermaleng.2017.08.009>.
- [74] Mantripragada HC, Rubin ES. Calcium looping cycle for CO₂ capture - performance, cost and feasibility analysis. *Energy Proc* 2013;63:2199–206. <https://doi.org/10.1016/j.egypro.2014.11.239>.
- [75] ZEP. The costs of CO₂ capture, transport and storage. European Technology Platform for Zero Emission Fossil Fuel Power Plants; 2011.
- [76] Versteeg P, Rubin ES. A technical and economic assessment of ammonia-based post-combustion CO₂ capture at coal-fired power plants. *Int J Greenh Gas Control* 2011;5:1596–605. <https://doi.org/10.1016/j.ijggc.2011.09.006>.
- [77] Mac Dowell N, Shah N. The multi-period optimisation of an amine-based CO₂ capture process integrated with a super-critical coal-fired power station for flexible operation. *Comput Chem Eng* 2015;74:169–83. <https://doi.org/10.1016/j.compchemeng.2015.01.006>.
- [78] Rubin ES, Davison JE, Herzog HJ. The cost of CO₂ capture and storage. *Int J Greenh Gas Control* 2015;40:378–400. <https://doi.org/10.1016/j.ijggc.2015.05.018>.
- [79] Berstad D, Anantharaman R, Jordal K. Post-combustion CO₂ capture from a natural gas combined cycle by CaO/CaCO₃ looping. *Int J Greenh Gas Control* 2012;11:25–33. <https://doi.org/10.1016/j.ijggc.2012.07.021>.
- [80] Hu Y, Ahn H. Process integration of a calcium-looping process with a natural gas combined cycle power plant for CO₂ capture and its improvement by exhaust gas recirculation. *Appl Energy* 2017;187:480–8. <https://doi.org/10.1016/j.apenergy.2016.11.014>.
- [81] Biliyok C, Yeung H. Evaluation of natural gas combined cycle power plant for post-combustion CO₂ capture integration. *Int J Greenh Gas Control* 2013;19:396–405. <https://doi.org/10.1016/j.ijggc.2013.10.003>.
- [82] Cormos CC. Assessment of chemical absorption/adsorption for post-combustion CO₂ capture from natural gas combined cycle (NGCC) power plants. *Appl Therm Eng* 2015;82:120–8. <https://doi.org/10.1016/j.applthermaleng.2015.02.054>.
- [83] Cormos CC, Cormos AM. Assessment of CO₂ capture by calcium looping from natural gas combined cycle (NGCC) power plants. *Chem Eng Trans* 2015;45:277–82. <https://doi.org/10.3303/CET1545047>.
- [84] Erans M, Hanak DP, Mir J, Anthony EJ, Manovic V. Process modelling and techno-economic analysis of natural gas combined cycle integrated with calcium looping. *Therm Sci* 2016;20:59–67. <https://doi.org/10.2298/TSCI151001209E>.
- [85] CCC. Next steps for UK heat policy. London, UK: Committee on Climate Change; 2016.
- [86] Wu W, Chen SC, Kuo PC, Chen SA. Design and optimization of stand-alone triple combined cycle systems using calcium looping technology. *J Clean Prod* 2017;140:1049–59. <https://doi.org/10.1016/j.jclepro.2016.10.079>.
- [87] Zhu L, Chen H, Fan J, Jiang P. Thermo-economic investigation: an insight tool to analyze NGCC with calcium-looping process and with chemical-looping combustion for CO₂ capture. *Int J Energy Res* 2016;40:1908–24. <https://doi.org/10.1002/er.3556>.
- [88] Wiranarongkorn K, Arpornwathanon A. Analysis of the Ca-looping sorption-enhanced steam reforming and solid oxide fuel cell integrated process using bio-oil. *Energy Convers Manag* 2017;134:156–66. <https://doi.org/10.1016/j.enconman.2016.12.025>.
- [89] Wiranarongkorn K, Im-Orb K, Ponpesh P, Patcharavorachot Y, Arpornwathanon A. Design and evaluation of the sorption-enhanced steam reforming and solid oxide fuel cell integrated system with anode exhaust gas recirculation for combined heat and power generation. *Chem Eng Trans* 2017;57. <https://doi.org/10.3303/CET1757017>.
- [90] Martínez I, Murillo R, Grasa G, Fernández JR, Abanades JC. Integrated combined cycle from natural gas with CO₂ capture using a Ca-Cu chemical loop. *AIChE J* 2013;59:2780–94. <https://doi.org/10.1002/aic.14054>.
- [91] Diglio G, Hanak DP, Bareschino P, Mancusi E, Pepe F, Montagnaro F, et al. Techno-economic analysis of sorption-enhanced steam methane reforming in a fixed bed reactor network integrated with fuel cell. *J Power Sources* 2017;364:41–51. <https://doi.org/10.1016/j.jpowsour.2017.08.005>.
- [92] Rubin ES, Chen C, Rao AB. Cost and performance of fossil fuel power plants with CO₂ capture and storage. *Energy Policy* 2007;35:4444–54. <https://doi.org/10.1016/j.enpol.2007.03.009>.
- [93] Kanniche M, Gros-Bonnivard R, Jaud P, Valle-Marcos J, Amann JM, Bouallou C. Pre-combustion, post-combustion and oxy-combustion in thermal power plant for CO₂ capture. *Appl Therm Eng* 2010;30:53–62. <https://doi.org/10.1016/j.applthermaleng.2009.05.005>.
- [94] Chiesa P, Lozza G, Mazzocchi L. Using hydrogen as gas turbine fuel. *J Eng Gas Turbines Power* 2005;127:73–80. <https://doi.org/10.1115/1.1787513>.
- [95] Symonds RT, Lu DY, Manovic V, Anthony EJ. Pilot-scale study of CO₂ capture by CaO-based sorbents in the presence of steam and SO₂. *Ind Eng Chem Res* 2012;51:7177–84. <https://doi.org/10.1021/ie2030129>.
- [96] Strelow M, Schlitzberger C, Röder F, Magda S, Leithner R. CO₂ separation by carbonate looping including additional power generation with a CO₂-H₂O steam turbine. *Chem Eng Technol* 2012;35:431–9. <https://doi.org/10.1002/ceat.201100463>.
- [97] Lara Y, Martínez A, Lisbona P, Romeo LM. Heat integration of alternative Ca-looping configurations for CO₂ capture. *Energy* 2016;116:956–62. <https://doi.org/10.1016/j.energy.2016.10.020>.
- [98] Song C, Liu Q, Ji N, Deng S, Zhao J, Li Y, et al. Alternative pathways for efficient CO₂ capture by hybrid processes - a review. *Renew Sustain Energy Rev* 2018;82:215–31. <https://doi.org/10.1016/j.rser.2017.09.040>.
- [99] Romano MC. Ultra-high CO₂ capture efficiency in CFB oxyfuel power plants by calcium looping process for CO₂ recovery from purification units vent gas. *Int J Greenh Gas Control* 2013;18:57–67. <https://doi.org/10.1016/j.ijggc.2013.07.002>.
- [100] Ortiz C, Valverde JM, Chacartegui R, Benítez-Guerrero M, Perejón A, Romeo LM. The oxy-CaL process: a novel CO₂ capture system by integrating partial oxy-combustion with the calcium-looping process. *Appl Energy* 2017;196:1–17. <https://doi.org/10.1016/j.apenergy.2017.03.120>.
- [101] Li Y, Zhao C, Ren Q. Thermodynamic simulation of CO₂ capture for an IGCC power plant using the calcium looping cycle. *Chem Eng Technol* 2011;34:946–54. <https://doi.org/10.1002/ceat.201000384>.
- [102] Cormos CC. Economic implications of pre- and post-combustion calcium looping configurations applied to gasification power plants. *Int J Hydrogen Energy* 2014;39:10507–16. <https://doi.org/10.1016/j.ijhydene.2014.05.033>.
- [103] Chen S, Wang D, Xue Z, Sun X, Xiang W. Calcium looping gasification for high-concentration hydrogen production with CO₂ capture in a novel compact fluidized bed: simulation and operation requirements. *Int J Hydrogen Energy* 2011;36:4887–99. <https://doi.org/10.1016/j.ijhydene.2010.12.130>.
- [104] Cormos C-C, Cormos A-M. Assessment of calcium-based chemical looping options for gasification power plants. *Int J Hydrogen Energy* 2013;38:2306–17. <https://doi.org/10.1016/j.ijhydene.2012.11.128>.
- [105] Wang D, Chen S, Xu C, Xiang W. Energy and exergy analysis of a new hydrogen-fueled power plant based on calcium looping process. *Int J Hydrogen Energy* 2013;38:5389–400. <https://doi.org/10.1016/j.ijhydene.2013.02.060>.
- [106] Chiesa P, Consonni S. Shift reactors and physical absorption for low-CO₂ emission IGCCs. *J Eng Gas Turbines Power* 1999;121:295–305. <https://doi.org/10.1115/1.2817120>.
- [107] Fiaschi D, Lombardi L, Sergio E. Integrated gasifier combined cycle plant with integrated CO₂-H₂S removal: performance analysis, life cycle assessment and energetic life cycle assessment. *Int J Appl Thermodyn* 2002;5:13–24.
- [108] Zhu L, Jiang P, Fan J. Comparison of carbon capture IGCC with chemical-looping combustion and with calcium-looping process driven by coal for power

- generation. *Chem Eng Res Des* 2015;104:110–24. <https://doi.org/10.1016/j.cherd.2015.07.027>.
- [109] Connell DP, Lewandowski DA, Ramkumar S, Phalak N, Statnick RM, Fan L-S. Process simulation and economic analysis of the calcium looping process (CLP) for hydrogen and electricity production from coal and natural gas. *Fuel* 2013;105:383–96. <https://doi.org/10.1016/j.fuel.2012.07.006>.
- [110] Black J. Cost and performance baseline for fossil energy plants volume 1: Bituminous coal and natural gas to electricity. DOE/2010/1. Pittsburgh, PA, USA: National Energy Technology Laboratory; 2013.
- [111] Kunze C, De S, Spliethoff H. A novel IGCC plant with membrane oxygen separation and carbon capture by carbonation-calcinations loop. *Int J Greenh Gas Control* 2011;5:1176–83. <https://doi.org/10.1016/j.ijggc.2011.05.038>.
- [112] Miller BG. Clean coal engineering technology. Burlington, MA, USA: Butterworth-Heinemann; 2011.
- [113] IEA. CO₂ emissions from fuel combustion - highlights. Paris, France: IEA Publications; 2012.
- [114] Chi J, Zhao L, Wang B, Li Z, Xiao Y, Duan Y. Thermodynamic performance assessment and comparison of IGCC with solid cycling process for CO₂ capture at high and medium temperatures. *Int J Hydrogen Energy* 2014;39:6479–91. <https://doi.org/10.1016/j.ijhydene.2014.02.005>.
- [115] Hanak DP, Jenkins BG, Kruger T, Manovic V. High-efficiency negative-carbon emission power generation from integrated solid-oxide fuel cell and calciner. *Appl Energy* 2017;205:1189–201. <https://doi.org/10.1016/j.apenergy.2017.08.090>.
- [116] Romano MC, Lozza GG. Long-term coal gasification-based power with near-zero emissions. Part B: Zecomag and oxy-fuel IGCC cycles. *Int J Greenh Gas Control* 2010;4:469–77. <https://doi.org/10.1016/j.ijggc.2009.11.010>.
- [117] Romano MC, Lozza GG. Long-term coal gasification-based power plants with near-zero emissions. Part A: Zecomix cycle. *Int J Greenh Gas Control* 2010;4:459–68. <https://doi.org/10.1016/j.ijggc.2009.11.009>.
- [118] Siefert NS, Chang BY, Litster S. Exergy and economic analysis of a CaO-looping gasifier for IGFC-CCS and IGCC-CCS. *Appl Energy* 2014;128:230–45. <https://doi.org/10.1016/j.apenergy.2014.04.065>.
- [119] Emami-Taba I, Irfan MF, Wan Daud WMA, Chakrabarti MH. Fuel blending effects on the co-gasification of coal and biomass - a review. *Biomass Bioenergy* 2013;57:249–63. <https://doi.org/10.1016/j.biombioe.2013.02.043>.
- [120] Starfelt F, Tomas Aparicio E, Li H, Dotzauer E. Integration of torrefaction in CHP plants - a case study. *Energy Convers Manag* 2015;90:427–35. <https://doi.org/10.1016/j.enconman.2014.11.019>.
- [121] Kuo P-C, Wu W. Design and thermodynamic analysis of a hybrid power plant using torrefied biomass and coal blends. *Energy Convers Manag* 2016;111:15–26. <https://doi.org/10.1016/j.enconman.2015.12.021>.
- [122] Yan L, He B. On a clean power generation system with the co-gasification of biomass and coal in a quadruple fluidized bed gasifier. *Bioresour Technol* 2017;235:113–21.
- [123] Diglio G, Hanak DP, Bareschino P, Pepe F, Montagnaro F, Manovic V. Modelling of sorption-enhanced steam methane reforming in a fixed bed reactor network integrated with fuel cell. *Appl Energy* 2018;210:1–15. <https://doi.org/10.1016/j.apenergy.2017.10.101>.
- [124] Fout T, Zoelle A, Keairns D, Turner M, Woods M, Kuehn N, et al. Cost and performance baseline for fossil energy plants volume 1a: bituminous coal (PC) and natural gas to electricity. Pittsburgh, PA, USA: National Energy Technology Laboratory; 2015.
- [125] Velumani S, Guzman CE, Peniche R, Vega R. Proposal of a hybrid CHP system: SOFC/microturbine/absorption chiller. *Int J Energy Res* 2010;34:1088–95. <https://doi.org/10.1002/er.1632>.
- [126] Facci AL, Cigolotti V, Jannelli E, Ubertini S. Technical and economic assessment of a SOFC-based energy system for combined cooling, heating and power. *Appl Energy* 2017;192:563–74. <https://doi.org/10.1016/j.apenergy.2016.06.105>.
- [127] Scataglini R, Mayyas A, Wei M, Han Chan S, Lipman T, Gosselin D, et al. A total cost of ownership model for solid oxide fuel cells in combined heat and power and power-only applications. Berkeley, CA, USA: Lawrence Berkeley National Laboratory; 2015.
- [128] ECOFYS. International comparison of fossil power efficiency and CO₂ intensity - Update 2014. Utrecht, Netherlands: ECOFYS Netherlands B.V.; 2014.
- [129] EIA. Electric power annual 2016. Washington, DC, USA: US Department of Energy; 2017.
- [130] IEA. Tracking clean energy progress 2013. IEA input to the clean energy ministerial. Paris, France: IEA Publications; 2013.
- [131] IEA. High-efficiency power generation - review of alternative systems. London, UK: IEA Clean Coal Centre; 2015.
- [132] Gonzalez-Salazar MA, Kirsten T, Prchlik L. Review of the operational flexibility and emissions of gas- and coal-fired power plants in a future with growing renewables. *Renew Sustain Energy Rev* 2018;82:1497–513. <https://doi.org/10.1016/j.rser.2017.05.278>.
- [133] Stanger R, Wall T, Spörl R, Paneru M, Grathwohl S, Weidmann M, et al. Oxyfuel combustion for CO₂ capture in power plants. *Int J Greenh Gas Control* 2015;40:55–125. <https://doi.org/10.1016/j.ijggc.2015.06.010>.
- [134] Liang Z (Henry), Rongwong W, Liu H, Fu K, Gao H, Cao F, et al. Recent progress and new developments in post-combustion carbon-capture technology with amine based solvents. *Int J Greenh Gas Control* 2015;40:26–54. <https://doi.org/10.1016/j.ijggc.2015.06.017>.
- [135] Hanak DP, Powell D, Manovic V. Techno-economic analysis of oxy-combustion coal-fired power plant with cryogenic oxygen storage. *Appl Energy* 2017;191:193–203. <https://doi.org/10.1016/j.apenergy.2017.01.049>.
- [136] Cormos CC. Oxy-combustion of coal, lignite and biomass: a techno-economic analysis for a large scale carbon capture and storage (CCS) project in Romania. *Fuel* 2016;169:50–7. <https://doi.org/10.1016/j.fuel.2015.12.005>.



DSPACE

<https://dspace.org/>

From post-combustion carbon capture to sorption-enhanced hydrogen production: A state-of-the-art review of carbonate looping process feasibility

Hanak, Dawid P.; Michalski, Sebastian; Manovic, Vasilije

2018-10-04

Elsevier

<https://doi.org/10.1016/j.enconman.2018.09.058>

Dawid Hanak, Sebastian Michalski and Vasilije Manovic. From post-combustion carbon capture to sorption-enhanced hydrogen production: A state-of-the-art review of carbonate looping process feasibility. Energy Conversion and Management, Volume 177, 1 December 2018, Pages 428-452